



# PRACTICAL HYDRAULICS.



# PRACTICAL HYDRAULICS:

A SERIES

OR

## RULES AND TABLES

FOR

THE USE OF ENGINEERS, ETC., ETC.

BY

THOMAS BOX,

*Author of "PRACTICAL TREATISE ON HEAT," "MILL-CARING," ETC.*

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SEVENTH EDITION.

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## PREFACE TO THE SECOND EDITION

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In preparing a Second Edition of 'Practical Hydraulics' considerable alterations and additions have been made. To facilitate reference, the work has been divided into Chapters, additional Rules for Culverts and other subjects have been given, including several new Tables, and an increased number of Illustrations. These alterations were so considerable, that it was found necessary to re-write the whole, and thus opportunity was given to introduce much new and valuable information, which, it is hoped, will increase the usefulness of the work.

BATH, July, 1870

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## PREFACE TO THE FIRST EDITION

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This reader must not expect, in this little book, an exhaustive treatise on Hydraulics, many such have been written, and they leave little or nothing to be desired. This work consists of a series of Rules and Tables, giving unusual facility for the solution of questions which occur in the daily practice of Engineers.

For the two leading questions—the Discharge of Pipes, and of Open Channels—two sets of Tables are given, the reason for

which may not be obvious; but it is impossible to give Tables combining extreme facility with extreme accuracy for low heads, and the author has therefore given two Tables, one giving accurate results in all ordinary cases with the least possible labour, and the other giving, with more labour, exact results in extreme cases.

For the most part the Rules and Tables have been long used in an extensive practice, and the principal reason for publishing them is the author's desire that the profession from which he has retired may have the benefit of Tables, &c., which for many years have been very useful to himself.

EASEDALE, GRASMERE,

*July, 1867.*

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# PRACTICAL HYDRAULICS.

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## CHAPTER I.

### DISCHARGE OF APERTURES, PIPES, &c

(1) "*Velocity of Efflux*"—The velocity with which water issues from the side of a vessel, as at A, Fig. 1, is the same as that of a body falling freely by gravity from the height H, or the distance from the centre of the orifice to the surface of the water. This velocity is given by the rule —

$$V = \sqrt{H} \times 8$$

In which H = the height or head of water in feet, and V = the velocity in feet per second. From this we may obtain another rule giving the discharge in gallons, which becomes —

$$G = \sqrt{H} \times d^2 \times 16.3$$

In which H = the head of water in feet, d = the diameter of the orifice in inches, and G = gallons discharged per minute. Table 1 has been calculated by this rule.

These rules give the *theoretical* velocity and discharge for application to practice, they may require some modification to adapt them to the particular form of the orifice.

(2) "*Discharge by an Orifice in a Thin Plate*" — It has been found by experiment that, when the discharging orifice is made in a thin plate, the converging currents of water approaching the aperture cause a *contraction* in the issuing stream, so that instead of a parallel or cylindrical jet, it becomes a conical one of the form shown by Fig. 2, the greatest contraction being at

TABLE I.—Of the THEORETICAL DISCHARGE of WATER by ROUND APERTURES of various DIAMETERS, and under different Heads of Water Pressure

THEORETICAL DISCHARGE OF APERTURES.

Diam. in inch	HEAD OF WATER IN FEET.												24		
	1	2	3	4	5	6	7	8	9	10	12	14			
1	4.7	6.6	8.1	9.4	10.5	11.5	12.4	13.3	14.1	14.8	16.2	17.6	21	22	23
2	16.8	26.1	37.6	42.0	49.6	53.2	56.4	59.2	61.8	70.4	75.2	79.6	84	88	92
3	42.2	59.1	72.9	81.6	94.5	103	112	120	127	133	146	158	169	179	207
4	73.2	106	130	150	168	184	198	213	225	237	259	281	301	318	368
5	117	163	203	235	262	287	310	332	352	370	405	440	470	497	550
6	169	237	291	328	378	414	446	479	507	533	583	633	677	716	758
7	22.0	31.0	39.7	46.0	51.4	56.3	60.7	65.2	69.1	72.5	75.4	80.2	82.1	875	1029
8	49.1	62.2	71.8	80.1	87.2	92.0	97.0	102.0	107.0	112.0	117.0	122.0	127.0	132.0	157.0
9	59.1	65.1	75.0	81.0	87.0	93.0	99.0	105.0	110.0	114.9	119.0	123.0	127.3	134.4	147.2
10	170	26.0	31.0	39.0	49.0	59.0	69.0	79.0	89.0	99.0	109.0	119.0	129.0	139.0	157.0
12	67.6	97.2	116.8	135.3	151.2	165.6	178.5	191.5	203.0	213.1	233.3	253.4	270.7	286.5	302.4
14	120.1	154.8	184.2	205.8	225.4	245.0	266.6	276.4	290.1	317.5	345.0	368.4	390.0	411.6	431.2
16	120.1	167.0	207.4	240.6	268.8	294.4	317.4	340.5	361.0	378.9	414.7	450.6	481.3	509.4	537.6
18	159.1	213.9	262.4	301.5	340.2	372.6	401.8	430.9	456.8	479.5	52.19	570.2	609.1	644.7	680.4
20	168.0	261.0	324.0	376.0	420.0	460.0	490.0	532.0	561.0	592.0	618.0	704.0	752.0	796.0	840.0
22	227.5	319.1	392.0	455.0	508.2	550.6	600.2	643.7	682.4	716.3	781.1	851.8	903.9	963.2	1016.1
24	270.1	380.9	467.2	511.4	601.8	662.4	714.0	766.0	812.0	853.6	913.2	1013.6	1082.9	1146.0	1205.6
30	423.0	591.0	72.0	81.0	91.5	103.5	111.0	119.7	126.9	133.2	145.5	155.0	169.2	179.1	198.0
36	2.32	3.275	4.01	4.63	5.18	5.67	6.13	6.55	6.95	7.32	8.03	8.67	9.27	9.83	10.36

Mean  
in  
inch

the point C, whose distance from the plate is half the diameter of the orifice, and its diameter 78 $\frac{1}{4}$ , that of the orifice being 1. The form from B to C may be taken as a curve, whose radius is 1.22 times the diameter of the orifice.

Now, the foregoing rule gives the maximum velocity, or that at the point of greatest contraction C, and if the diameter be taken there, the rules would give the true velocity and discharge without correction. But it is obvious that the velocity at the aperture itself (or at B) would be less than at C in the ratio of the respective areas at the two points, or as 1 $\frac{1}{2}$  to 78 $\frac{1}{4}$  or 1 to 61.5, and in that case, the diameter being taken at B, the velocity there would become  $V = \sqrt{H} \times 8 \times 61.5$  and the discharge  $G = \sqrt{H} \times d^2 \times 16.3 \times 61.5$ . From this we get for apertures in a thin plate, the rules —

$$G = \sqrt{H} \times d^2 \times 10$$

$$H = \left( \frac{G}{d^2 \times 10} \right)^2$$

$$d = \left( \frac{G}{\sqrt{H} \times 10} \right)^{\frac{1}{2}}$$

Thus, with 3 inches diameter and 16 feet head, the discharge would be  $\sqrt{16} \times 3^2 \times 10$  or  $4 \times 9 \times 10 = 360$  gallons per minute. The head for 150 gallons per minute with 2 inches diameter  $= \left( \frac{150}{4 \times 10} \right)^2 = 14.06$  feet, and the diameter for 200 gallons per minute with 20 feet head would be  $\left( \frac{200}{4 \cdot 47 \times 10} \right)^{\frac{1}{2}} = 2 \cdot 11$  inches, &c., &c.

(3) "Discharge by Short Tubes" — When the aperture is of considerable thickness or has the form of a short tube not less in length than twice the diameter, the amount of contraction is found to be less and the discharge greater, than with a thin plate. Fig. 3 shows a tube 1 inch diameter and 2 inches long, the greatest contraction is in that case 9 inch diameter, and its pro-

proportional area  $\cdot 9^2 = \cdot 81$ , or say  $\cdot 8$  of the area of the tube. For short tubes therefore the rules become:—

$$G = \sqrt{H} \times d^2 \times 13$$

$$H = \left( \frac{G}{d^2 \times 13} \right)^2$$

$$d = \left( \frac{G}{\sqrt{H} \times 13} \right)^{\frac{1}{2}}$$

Table 2 has been calculated by these rules; thus, for a 7-inch pipe discharging 450 gallons, the Table shows that the head necessary to generate the velocity at entry is 6 inches; this is irrespective of friction, which, in fact, for so short a tube as the rule supposes, would be practically nothing. This Table applies to all cases of pipes; for instance, Fig. 4 shows the inlet end of a main from a reservoir, which will require for the velocity at entry alone the amount of head shown by the Table. When, as is usually the case, the pipe is of considerable length, the head due to friction must also be allowed for.

(1.) "Friction of Long Pipes."—With a long pipe there is not only the loss of head due to the velocity at entry, but also another loss due simply to the friction of the water against the sides of the pipe, so that in all cases the head consumed may be considered as composed of two portions:—one, the amount due to velocity of entry, irrespective of friction; and the other, the amount due to friction alone. Thus, in Fig. 8 the head  $H$  gives a certain velocity of discharge by the short pipe A; but to give the same velocity in the long main B C, the head  $H'$  is necessary, of which  $H'$  is consumed in generating the velocity at entry, being the same as for A, and the rest, or  $H$ , in the friction of the long pipe: the total head is, of course, the sum of the two.

(5.) The loss of head by friction may be calculated by the following rules:—

$$G = \left( \frac{(3d)^2 \times H}{L} \right)^{\frac{1}{2}}$$

$$H = \frac{G^2 \times L}{(3d)^2}$$

TABLE 2.—Of the Actual Discharge by Spill Terns of various Diameters, with Spill Edge up to 100 feet, Different Heads of Water Pressure, being 1/16th of the Theoretical Fall over.

Diam. in Inches	Head of Water in Feet.														
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
Distances in Various feet.															
1	3.76	5.28	6.48	7.52	8.4	9.2	9.9	10.6	11.3	11.8	12.0	12.2	12.4	12.6	12.8
2	15.01	21.25	30.1	31.6	36.8	39.7	42.6	45.1	47.4	51.4	52.2	53.2	54.2	55.2	56.2
3	51.8	47.5	58.3	67.7	73.6	82.4	89.6	96.0	101.6	106.4	109.4	112.4	115.4	118.4	121.4
4	60.2	58.8	101	120	129	147	159	170	179	188	197	206	215	224	233
5	93.0	132	162	183	210	230	248	262	276	290	294	304	314	324	334
6	135	106	233	270	302	331	357	382	406	426	446	466	486	506	526
7	191	218	318	308	411	470	446	521	533	520	538	529	531	527	521
8	241	939	414	481	538	580	631	681	722	753	784	815	846	877	908
9	305	427	525	609	680	745	803	863	911	969	1022	1070	1118	1159	1197
10	370	529	619	722	810	920	992	1063	1125	1181	1243	1304	1364	1424	1484
12	541	762	934	1082	1240	1325	1428	1522	1621	1727	1827	1927	2027	2127	2227
14	730	993	1268	1474	1616	1803	1914	2070	2227	2279	2464	2516	2564	2616	2664
15	816	1159	1458	1692	1870	2070	2252	2450	2644	2916	3104	3294	3484	3674	3864
16	902	1352	1659	1925	2130	2335	2539	2721	2883	3001	3114	3203	3303	3403	3503
18	1218	1710	2029	2436	2722	2981	3214	3412	3622	4122	4522	4922	5322	5722	6122
20	1504	2112	2592	3008	3360	3660	3963	4265	4512	4778	5161	5522	5816	6214	6593
22	1820	2552	3136	3610	4063	4432	4861	5113	5353	5770	6272	6711	7272	7772	8272
24	2163	3046	3737	4331	4838	5279	5771	6125	6496	6824	7143	7604	8064	8524	8984
30	3384	4752	5832	6768	7560	8250	8929	9576	10152	10656	11161	12272	13236	14260	15260

$$d = \left( \frac{G^2 \times L}{H} \right)^{\frac{1}{4}} \div 3$$

$$L = \frac{(3d)^4 \times H}{G^2}$$

In these rules  $d$  = diameter of the pipe in inches.

$L$  = length in yards.

$H$  = head of water in feet.

$G$  = gallons per minute.

These rules require the use of logarithms to work them easily: thus, to find the discharge by a 7-inch pipe 3797 yards long with 45 feet head, we have:—

$$7 \times 3 = 21 = 1 \cdot 322219$$

$$\quad \quad \quad 5$$

$$\overline{6 \cdot 611095}$$

$$\times 45 = \overline{1 \cdot 653218}$$

$$\overline{8 \cdot 261308}$$

$$\div 3797 = \overline{3 \cdot 579441}$$

$$\overline{2) 1 \cdot 684867}$$

$$\overline{2 \cdot 312133} = 220 \text{ gallons per minute.}$$

Again, to find the head necessary to discharge 320 gallons per minute by an 8-inch pipe 3157 yards long, we have:—

$$320 = 2 \cdot 505150$$

$$\quad \quad \quad 2$$

$$\overline{5 \cdot 010300}$$

$$\times 3157 = \overline{3 \cdot 636099}$$

$$\overline{8 \cdot 518999}$$

$$8 \times 3 = 21 = 1 \cdot 380211 \times 5 = \overline{6 \cdot 901055}$$

$$\overline{1 \cdot 617911} = 41 \cdot 46 \text{ feet head.}$$

And again, to find the diameter for 110 gallons per minute with 66 feet head, the length being 273 yards, we have:—

$$\begin{array}{r}
 110 = 2\ 041393 \\
 \quad \quad \quad 2 \\
 \hline
 \quad \quad \quad 4\ 082786 \\
 \times 273 = 2\ 436163 \\
 \hline
 \quad \quad \quad 6\ 518949 \\
 - 56 = 1\ 748188 \\
 \hline
 5) 1\ 770761 \\
 \quad \quad \quad 954152 = 9, \text{ and } \frac{9}{3} = 3 \text{ inches diameter}
 \end{array}$$

Table 3 has been calculated by these rules, and will greatly facilitate the calculation of pipe questions, it also has the great advantage of requiring only the simple rules of arithmetic.

(6) 1st Having G, L, and  $d$  given, to find H. In the Table opposite the given number of gallons, and under the given diameter, is found the head due to a length of one yard, and multiplying that number by the given length in yards, gives the required head of water in feet. Thus, taking our former illustration in (5), the head to deliver 320 gallons per minute by an 8-inch pipe 8457 yards long—opposite 320 gallons in the Table, and under 8 inches diameter, is .01286 feet, and  $.01286 \times 3457 = 44\ 46$  feet, the head sought.

(7) 2nd To find  $d$ , having H, L, and G given. Divide the given head of water in feet by the given length in yards, and the nearest number thereto in the Table opposite the given number of gallons will be found under the required diameter. Thus, to find, the diameter for 110 gallons per minute with 56 feet head, the length being 273 yards, we have  $\frac{56}{273} = .205$ , looking for which in the Table opposite 110 gallons we find it under 3 inches, the diameter sought (see 5). Again, to find the diameter for 320 gallons, 20 feet head, and 1600 yards long, we have  $\frac{20}{1600} = .0125$ , the nearest number to which, in the Table (.01286) is found under 8 inches, the diameter sought. In most cases the tabular number will not be the exact number.

## HEAD FOR FRICTION OF LONG PIPES -

TABLE 3.—Of the HEAD of WATER CONSUMED by Friction with Pipes 1 yard long

Gallons per Minute	DIAMETER of the Pipe in inches											
	1	1½	2	2½	3	3½	4	4½	5	6	7	8
	HEAD of WATER in Feet											
1	0.041	0.0054	0.0012	0.0032	0.00932	0.00932	0.00932	0.00932	0.00932	0.00932	0.00932	0.00932
2	0.164	0.0216	0.0051	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165
3	0.570	0.0457	0.0115	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279
4	0.659	0.0567	0.01905	0.00671	0.00671	0.00671	0.00671	0.00671	0.00671	0.00671	0.00671	0.00671
5	1.078	0.1354	0.0321	0.01053	0.01053	0.01053	0.01053	0.01053	0.01053	0.01053	0.01053	0.01053
6	1.481	0.1950	0.0513	0.01517	0.01517	0.01517	0.01517	0.01517	0.01517	0.01517	0.01517	0.01517
7	2.016	0.2655	0.0660	0.02064	0.02064	0.02064	0.02064	0.02064	0.02064	0.02064	0.02064	0.02064
8	2.633	0.3403	0.0823	0.02659	0.02659	0.02659	0.02659	0.02659	0.02659	0.02659	0.02659	0.02659
9	3.333	0.4369	0.1011	0.03113	0.03113	0.03113	0.03113	0.03113	0.03113	0.03113	0.03113	0.03113
10	4.11	0.5111	0.1280	0.04121	0.04121	0.04121	0.04121	0.04121	0.04121	0.04121	0.04121	0.04121
20	1.61	2.167	0.514	0.1635	0.1635	0.1635	0.1635	0.1635	0.1635	0.1635	0.1635	0.1635
30	3.70	4.877	1.15	0.3792	0.3792	0.3792	0.3792	0.3792	0.3792	0.3792	0.3792	0.3792
40	6.58	8.070	2.05	0.6742	0.6742	0.6742	0.6742	0.6742	0.6742	0.6742	0.6742	0.6742
50	10.23	1.35	321	1.053	1.053	1.053	1.053	1.053	1.053	1.053	1.053	1.053
60	14.81	1.95	4.63	1.517	1.517	1.517	1.517	1.517	1.517	1.517	1.517	1.517
70	20.16	2.65	630	2.964	2.964	2.964	2.964	2.964	2.964	2.964	2.964	2.964
80	25.33	3.46	823	3.696	3.696	3.696	3.696	3.696	3.696	3.696	3.696	3.696
90	33.33	4.39	1.011	3.113	3.113	3.113	3.113	3.113	3.113	3.113	3.113	3.113
	DIAMETER of the Pipe in inches											
5	6	7	8	9	10	11	12	13	14	15	16	17
10	0.00131	0.00032	0.00021	0.00012	0.000069	0.0000411	0.0000165	0.00000616	0.00000211	0.00000165	0.000000616	0.000000165
20	0.01526	0.00211	0.00037	0.00000	0.000113	0.0000578	0.00001616	0.00000616	0.00000211	0.000001616	0.000000616	0.0000001616
30	0.01159	0.00176	0.00072	0.00000	0.00191	0.000927	0.00003703	0.00001488	0.00000529	0.00000259	0.000001488	0.000000529
40	0.02003	0.00504	0.00372	0.00000	0.00314	0.001050	0.00004728	0.00001742	0.00000759	0.00000359	0.000001742	0.000000759
50	0.03892	0.01393	0.00612	0.00000	0.00152	0.002569	0.0001481	0.0000615	0.00002659	0.00001155	0.00000569	0.000002659
60	0.07141	0.01205	0.00881	0.00000	0.00200	0.00415	0.001481	0.000615	0.000200	0.0001155	0.0000569	0.0000200
70	0.09613	0.02303	0.01567	0.00000	0.00563	0.00860	0.00415	0.001481	0.000563	0.0002659	0.0001155	0.0000563
80	0.085123	0.01286	0.01983	0.00000	0.01017	0.005615	0.002659	0.001481	0.0005615	0.0002659	0.0001155	0.00005615
90	0.10617	0.01286	0.01983	0.00000	0.01017	0.005615	0.002659	0.001481	0.0005615	0.0002659	0.0001155	0.00005615

Note.—For intermediate numbers, see body of general Table 3 as explained in (1) page 16.

## Hannibal's Tare 3—continued.

Gallons per Minute.	Rate of Water Flow.								
	1	14	2	21	3	31	4	5'	6
100	41.1	5.1	1.28	1.35	1.21	0.96	0.78	0.64	0.52
110	49.7	6.5	1.42	1.52	1.37	1.12	0.91	0.75	0.63
120	57.2	7.8	1.57	1.67	1.46	1.22	1.02	0.85	0.72
130	65.5	9.1	1.72	1.82	1.62	1.37	1.17	0.97	0.84
140	73.0	10.6	1.87	1.98	1.78	1.53	1.31	1.11	0.98
150	80.5	12.1	2.02	2.12	1.91	1.76	1.56	1.36	1.23
160	88.0	13.9	2.17	2.27	2.06	1.89	1.69	1.49	1.36
170	95.3	15.0	2.31	2.41	2.17	1.96	1.76	1.56	1.43
180	103.3	17.5	2.46	2.56	2.32	2.12	1.92	1.72	1.59
190	111.5	19.5	2.61	2.71	2.41	2.21	1.91	1.71	1.58
200	119.0	21.0	2.76	2.86	2.65	2.45	2.15	1.95	1.82
210	126.4	23.8	2.91	3.01	2.79	2.59	2.29	2.09	1.96
220	134.1	26.2	3.06	3.16	2.94	2.74	2.44	2.24	2.11
230	141.6	28.0	3.20	3.30	3.08	2.88	2.58	2.38	2.25
240	149.0	31.2	3.35	3.45	3.23	3.03	2.73	2.53	2.40
250	157.1	33.8	3.50	3.60	3.38	3.18	2.88	2.68	2.55
260	165.1	36.6	3.65	3.75	3.53	3.33	3.03	2.83	2.70
270	172.9	39.5	3.80	3.90	3.68	3.48	3.18	2.98	2.85
280	180.6	42.4	3.95	4.05	3.83	3.63	3.33	3.13	3.00
290	188.0	45.5	4.10	4.20	3.98	3.78	3.48	3.28	3.15
300	195.3	48.7	4.25	4.35	4.03	3.83	3.53	3.33	3.20
310	202.5	52.0	4.40	4.50	4.18	3.98	3.68	3.48	3.35

Hydraulic Table 3—continued

Gallons per minute.	Diameter of the Pipe in Inches								
	1	1½	2	2½	3	3½	4	5	6
HEAD OF WATER IN FEET									
320	421.3	55.5	13.16	4.315	1.734	.802	.4115	.13486	.054190
330	418.1	59.0	14.00	4.583	1.814	.853	.4376	.14312	.057630
340	475.6	62.6	14.87	4.871	1.959	.905	.4645	.15224	.061175
350	504.0	66.3	15.75	5.162	2.075	.959	.4923	.16133	.064627
360	533.3	70.2	16.60	5.461	2.196	1.015	.5248	.17068	.068584
370	563.3	74.1	17.60	5.763	2.330	1.072	.5502	.18029	.072447
380	594.2	78.2	18.57	6.055	2.446	1.131	.5803	.19017	.076416
390	625.8	82.4	19.50	6.409	2.576	1.191	.6112	.20031	.080431
400	658.4	86.7	20.57	6.742	2.710	1.253	.6430	.21072	.084672
410	691.7	91.0	21.61	7.083	2.847	1.317	.6755	.22138	.088958
420	725.8	95.5	22.68	7.433	2.988	1.382	.7080	.23231	.093350
430	760.8	100.1	23.8	7.773	3.113	1.448	.743	.2435	.09784
440	796.6	104.9	24.9	8.115	3.27	1.516	.778	.2549	.10245
450	833.2	109.7	26.0	8.553	3.443	1.586	.813	.2656	.10716
460	870.7	114.6	27.2	8.91	3.58	1.657	.850	.2786	.11197
470	909.0	113.7	28.4	3.30	3.74	1.730	.887	.2909	.11690
480	948.0	124.8	29.6	3.70	3.90	1.805	.925	.3034	.12192
490	988.0	130.1	30.8	4.11	4.06	1.891	.964	.3162	.059412
500	1028.7	135.4	32.1	4.53	4.23	1.953	1.004	.3292	.12706
520	1112.7	146.5	34.7	11.39	4.58	2.118	1.086	.3561	.13230
540	1200.0	158.0	37.5	12.28	4.93	2.284	1.171	.3810	.14313
560	1290.4	163.9	40.3	13.21	5.31	2.157	1.250	.4130	.16595

HYDRAULIC TABLE 3—continued

Gallons per Minute.	DIAMETER OF THE PIPE IN INCHES.								
	1	1½	2	2½	3	3½	4	5	6
550	1381.2	182.2	132	14.17	5.00	2.635	1.951	1.430	1.0238
600	1481.4	195.0	14.3	15.17	6.09	2.820	1.416	1.4741	1.0231
620	1581.8	208.3	19.4	16.19	6.51	3.011	1.514	1.5062	1.0236
650	1685.5	222.0	52.6	17.26	6.93	3.203	1.616	1.5394	1.0250
660	1732.5	236.0	56.0	18.35	7.37	3.112	1.720	1.5736	1.0255
680	1802.7	250.5	59.4	19.18	7.83	3.022	1.838	1.6089	1.0262
700	2016.3	275.5	63.0	20.04	8.30	3.870	1.909	1.6153	1.0266
720	2183.2	280.9	66.0	21.84	8.78	4.061	2.009	1.6295	1.0270
740	2255.3	296.7	70.4	23.07	9.44	4.260	2.200	1.6451	1.0274
760	2370.8	313.0	74.2	24.34	9.78	4.525	2.321	1.6600	1.0278
800	2503.5	329.6	78.2	25.03	10.30	4.760	2.445	1.6899	1.0282
820	2713.6	346.8	82.3	26.96	10.84	5.014	2.572	1.7190	1.0286
840	2777.9	364.3	86.4	28.13	11.39	5.268	2.702	1.7583	1.0290
860	2803.5	382.3	90.7	29.73	11.95	5.529	2.835	1.7972	1.0294
880	3013.1	400.7	95.5	31.16	12.52	5.791	2.972	1.8362	1.0298
900	3186.6	419.6	99.5	32.63	13.11	6.067	3.112	1.8755	1.0302
920	3373.1	438.9	104.1	31.13	12.72	6.316	3.255	1.9157	1.0306
940	3562.9	458.6	109.8	35.06	14.38	6.631	3.401	1.9547	1.0310
960	3753.0	478.8	113.6	37.23	14.96	6.923	3.551	1.9937	1.0314
980	3942.4	499.4	118.5	38.83	15.61	7.220	3.703	2.0327	1.0318
1000	4115.0	511.9	128.6	42.14	16.31	7.521	3.859	2.0718	1.0322

Hydraulic Table 3--continued.

Diameter of the Pipe in Inch.	Head or Water in Feet						
	10	12	14	15	16	18	20
100	000111	000165	0000755	0000541	0000302	0000217	0000158
110	000117	000200	0000635	0000471	0000263	0000155	0000100
120	000123	000238	0001161	0000780	0000535	0000313	0000153
130	000129	000253	0001232	0000915	0000623	0000368	0000145
140	000135	000271	0001133	0001062	0000730	0000217	0000170
150	000142	000273	0001352	0001121	0000819	0000252	0000197
160	000148	000279	0001233	0001133	0000832	0000290	0000116
170	000154	000285	0001193	0001177	0000864	0000357	0000230
180	000161	000300	0001221	0002156	0001121	0000629	0000257
190	000168	000311	0001219	0001755	0001270	0000705	0000371
200	000174	000316	0001219	0001936	0001116	0000786	0000316
210	000181	000320	0001200	0002167	0001549	0000571	0000164
220	000187	000325	0001191	0002389	0001739	0000930	0000567
230	000194	000329	0001181	0002622	0001839	0001051	0000411
240	000201	000330	0001171	0003103	0002866	0000571	0000227
250	000207	000335	0001171	0003117	0003076	0001152	00002501
260	000214	000337	0001171	0003121	0003220	0001254	0000533
270	000220	000342	0001171	0003139	0003397	0001361	0000650
280	000227	000345	0001171	0003172	0003662	0002653	0000680
290	000233	000347	0001171	0003205	0003950	0003537	0000691
300	000240	000352	0001171	0003236	0004218	0003676	0000710
310	000246	000355	0001171	0003298	0004535	0004177	0000734
320	000251	000357	0001171	0003355	0004857	0004631	0000750
330	000256	000360	0001171	0003488	0005187	0005200	0000789
340	000261	000363	0001171	0003620	0005507	0005831	0001051
350	000266	000365	0001171	0003753	0005827	0006157	0001157
360	000271	000368	0001171	0003885	0006187	0006500	0001235
370	000276	000371	0001171	0004018	0006520	0006831	0001316
380	000281	000374	0001171	0004153	0006857	0007200	0001451
390	000286	000377	0001171	0004288	0007187	0007532	0001535
400	000291	000380	0001171	0004423	0007520	0007871	0001626

## HEAD FOR FRICTION OF LONG PIPES

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Hydraulio Table 3—continued

Gallons per minute	Diameter of the Pipe in Inches.						
	10	12	14	15	16	18	20
HEAD OF WATER IN FEET							
001213	00193	0007872	0005519	0001018	0002210	0001316	0001032
001481	001800	0008332	0006501	0001273	0002371	0001400	0001097
110	001757	001911	0006815	0006261	0001535	0002517	0001186
1250	003011	002026	0009373	0006638	0001607	0002678	0001575
360	00333	002142	0009216	0007023	0005082	0002822	0001666
T-0	004537	002264	0001047	0007418	0005372	0002981	0001760
750	005912	002388	0007048	0007825	0005267	0003745	0001856
T-0	006200	002515	0011638	0008232	0005963	0003212	0001050
400	006584	002616	0012212	0008670	0006279	0003491	0002057
410	000917	002780	0012802	0009109	0006597	0003661	0002170
420	007259	002917	001337	0006559	0006923	0003911	0002268
430	00760	00705	001414	001002	000725	000102	000237
440	00770	00120	001481	001019	000759	000121	000248
450	00433	00334	001510	001097	000794	000141	000260
460	00570	00319	001619	001146	000830	000160	000272
470	00701	00365	001670	001197	000866	0001481	000284
480	00718	00791	001702	001218	0009301	000501	000296
490	00748	00397	001837	001301	000942	000522	000308
500	01023	00417	001912	001254	000981	000544	000321
520	01112	00447	002009	001464	001061	000588	000317
540	01200	00482	002231	001580	001144	000635	000371
560	01200	00518	002399	001639	001230	000103	000315

## HEAD FOR FRICTION OF LONG PIPES.

HYDRAULIC TABLE 3—continued

DRAWN BY THE FRIZZ IN FEET

DIAMETER IN. per inch	10	12	14	15	16	18	20	21	24
590	01591	002556	002571	001823	001220	000732	000432	000338	0001738
600	01591	002575	002751	001950	001412	000781	000462	000362	0001860
610	01591	002575	002751	002063	001508	000837	000494	000387	0001986
620	01591	002575	002751	002219	001607	000882	000526	000412	0002116
630	01782	00677	00131	002360	001709	000348	000500	000438	0002251
640	01902	00761	001535	002505	001814	001007	000524	000405	0002289
650	02010	00840	001549	002555	001933	001071	000630	000493	0002532
660	02133	00976	001566	002600	002032	001190	000666	000523	0002679
670	02251	00110	001120	002907	002151	001192	000704	000551	0002830
680	02370	00935	001110	003130	002266	001258	000742	000581	0002985
690	02489	00100	001655	002997	002387	001325	000782	000613	0003144
700	02607	01058	001857	00168	002511	001393	000823	000614	0003207
710	02725	01112	002043	002643	002638	001464	000668	000677	0003475
720	02843	01176	002253	003233	002769	001530	000935	000780	0004002
730	02961	01230	002550	004196	003038	001656	001011	000816	0004186
740	03079	01285	002859	004389	003178	001761	001088	000822	0004374
750	03197	01341	003251	005167	003274	001813	001041	000816	0004566
760	03315	01396	003601	005616	003616	002007	000710	000613	0004733
770	03433	01451	004004	006161	004167	002192	001136	000690	0004982
780	03551	01506	004351	006599	004610	002551	001051	000652	0005074
790	03669	01561	004730	007159	005167	003167	001361	000632	0005374
800	03787	01616	005176	007656	005756	003274	001610	000614	0005574
810	03905	01671	005576	008156	006156	003756	002008	000577	0005774
820	04023	01726	00603	01163	006823	004236	002502	000608	0006084
830	04141	01780	01285	01623	007253	004753	002902	000595	0005954
840	04259	01835	01339	01733	008233	005323	003038	000585	0005855
850	04377	01891	01394	02026	009233	006323	003756	000574	0005745
860	04495	01946	01447	02327	010256	007323	004236	000563	0005636
870	04613	02001	01503	02627	011258	008323	005123	000552	0005527
880	04731	02056	01555	02927	012256	009323	006123	000541	0005418
890	04849	02111	01606	03227	013258	010323	006923	000530	0005308
900	04967	02165	01657	03527	014258	011323	007823	000519	0005198
910	05085	02220	01711	03827	015258	012323	008723	000508	0005082
920	05203	02274	01756	04127	016258	015323	009623	000497	0004973
930	05321	02328	01811	04427	019258	018323	010523	000486	0004862
940	05439	02382	01855	04727	022258	021323	011423	000475	0004754
950	05557	02436	01909	05027	025258	020323	012523	000464	0004645
960	05675	02490	01953	05327	028258	023323	013623	000453	0004536
970	05793	02544	02004	05627	031258	028323	014723	000442	0004427
980	05911	02598	02049	05927	034258	031423	015823	000431	0004318
990	06029	02652	02103	06227	037258	038523	016923	000420	0004205
1000	06147	02706	02158	06527	040258	041723	018023	000409	0004098

HYDRAULIC TABLE 3—continued

Gallons per Minute.	DIAMETERS OF THE PIPES IN INCHES						12
	5	6	7	8	9	10	
2,000	5.2	2.11	.97	.59	.27	.171	.066
3,000	11.8	4.76	2.20	1.17	.62	.370	1.19
4,000	21.0	8.46	3.91	2.00	1.11	0.9	2.1
5,000	32.9	13.23	6.12	3.11	1.71	1.02	4.13
6,000	47.4	19.05	8.81	4.52	2.50	1.48	5.93
7,000	64.5	25.33	12.00	6.15	3.11	2.01	9.10
8,000	81.2	33.86	15.67	8.03	4.46	2.63	1.03
9,000	106.0	42.86	19.87	10.17	5.11	3.73	1.13
10,000	131.7	52.92	24.49	12.50	6.97	4.11	1.63
20,000	326.8	211.68	97.96	50.21	27.83	16.40	6.61
DIAMETERS OF THE PIPES IN MILLIMETERS							
14	15	16	17	18	19	20	21
HEAD OF WATER IN FEET							
2,000	0.010	0.016	0.027	0.037	0.054	0.074	0.110
3,000	0.033	0.047	0.063	0.087	0.115	0.150	0.230
4,000	0.063	0.087	0.127	0.163	0.203	0.261	-
5,000	0.101	0.135	0.181	0.219	0.271	0.321	0.431
6,000	0.155	0.205	0.241	0.281	0.342	0.412	0.572
7,000	0.274	0.365	0.492	0.671	0.830	1.093	-
8,000	0.469	0.619	0.817	1.139	1.523	2.044	-
9,000	0.699	0.939	1.237	1.766	2.314	3.010	-
10,000	1.065	1.511	2.092	2.717	3.428	4.100	-
20,000	3.06	2.16	1.56	0.871	0.514	0.403	-
30,000	6.88	4.67	3.53	1.96	1.15	.706	-
40,000	12.24	8.07	6.27	3.18	2.03	1.61	-
50,000	19.12	13.54	9.81	5.41	3.21	2.51	-
60,000	27.54	19.50	14.12	7.81	4.62	3.62	-
70,000	37.49	26.55	19.23	10.71	6.30	4.93	-
80,000	48.97	34.68	23.11	13.97	8.23	6.41	-
90,000	61.97	43.89	31.78	17.64	10.41	8.16	-
100,000	76.51	54.19	39.24	21.78	12.80	10.07	-

Note.—For intermediate numbers, see body of the General Table 3, as explained in (10) page 16.

desired, which will only show that the exact diameter is an odd size between the standard ones in the Table. But by the former rule in (6), this can be easily checked, thus in our case the true head for an 8 inch pipe would be  $01286 \times 1600 = 20\ 57$  feet instead of 20 feet, but, of course, in most cases 8 inches is near enough for practice.

(8) 3rd To find G, having H, L, and  $d$  given. Divide the given head of water in feet by the given length in yards, and the nearest number thereto in the Table, under the given diameter, will be found opposite the required number of gallons. Thus, to find the discharge of a 7-inch pipe 3797 yards long with 45 feet head, see (5), we have  $\frac{45}{3797} = 01185$ , and looking for this under 7 inches diameter, we find it opposite 220 gallons, the discharge sought. Again, for the discharge of a 10 inch pipe 3000 yards long with 40 feet head, we have  $\frac{40}{3000} = 01383$ , and the nearest number to that we find to be 01384 opposite 580 gallons, the discharge sought.

(9) 4th To find L, having H, G, and  $d$  given. Divide the given head by the head for one yard found in the Table under the given diameter, and opposite the given number of gallons, and the result is the required length. Thus, to determine the length of 4 inch pipe to consume 12 feet head with 130 gallons per minute, we find under 4 inches and opposite 130 gallons 0679 the head for one yard, and hence  $\frac{12}{0679} = 176$  yards, the length sought.

(10) To avoid a needless extension of the Table, we have given only the principal numbers from 1 to 90, and from 1000 to 100 000 gallons, leaving the intervening numbers to be supplied from the body of the general Table. In order to do this, it should be observed that the head varies as the square of the discharge, so that, for instance, ten times any given discharge will require 100 times the head, &c., &c. Thus, with 100 gallons, the Table shows that a 5 inch pipe requires 01317 foot

head per yard, then with 1000 gallons the head would be  
 $01317 \times 100 = 1\ 317$  foot, and with 10 gallons  $\frac{01317}{100} =$

0001317 foot The application of this principle to any case in practice is very simple say we require the head for 33 gallons with a  $2\frac{1}{2}$ -inch pipe 600 yards long Not finding 33 gallons in the Table, we take 330, the head for which is 4 589,

therefore for 33 gallons it will be  $\frac{4\ 589}{100} = 04589$  This may

be checked by the skeleton Table, which shows that 30 gallons require 03792 and 40 gallons 06742 foot, so that 04589 looks about right for 33 gallons Then the head required in our case is  $04589 \times 600 = 27\ 534$  feet

Again say we required the head for 2800 gallons with a 15 inch pipe 500 yards long Here we must take the head for 280 gallons from the Table, which is 0004248 for 2800 gallons, therefore, or 10 times the quantity, we should have

$0004248 \times 100 = 04248$  foot Checking this by the skeleton Table we find 0487 foot for 3000 gallons, showing that 04248 foot for 2800 gallons is about right Hence the head sought is, in our case,  $04248 \times 500 = 21\ 24$  feet

The same principle may be applied when the discharge is the unknown quantity, thus, to find the discharge of a  $2\frac{1}{2}$  inch pipe,

700 yards long with 17 feet head, we have  $\frac{17}{700} = 02428$ , which, by the skeleton Table, is somewhere between 20 and 30 gallons now, looking in the body of the Table between 200 and 300 gallons for the same figures (neglecting altogether for the moment the position of the decimal place) we find that the nearest to 2428 is 2427, which is opposite 240 gallons, 24 gallons is therefore the true discharge Again, to find the discharge of a pipe  $1\frac{1}{2}$  inch diameter, 200 yards long, with 4 5 feet head,

we have  $\frac{4\ 5}{200} = 0225$ , which, by Table, is between 6 and 7 gallons, now, looking between 600 and 700 gallons, we find the nearest to be 640 opposite 640 gallons, and as we know that

the true discharge is between 6 and 7 gallons, we infer that the exact quantity is 6.4 gallons, &c., &c.

(11) The 3rd illustration in (8) for finding G may be extended so as to give a useful general view of the discharge of different sized pipes with the same length and head. Thus, we found the tabular number for 3000 yards long and 40 feet head to be  $\frac{40}{3000} = .01333$ , and looking for this successively under different diameters we find that

A 6-inch pipe discharges 160 gallons per minute

7	"	235	"	"
8	"	330	"	"
9	"	440	"	"
10	"	580	"	"
12	"	900	"	&c

(12) "*Head for Velocity of Entry*"—To the head thus found by the preceding rules and Table, that due to velocity of entry has in all cases to be added, as explained in (4). When the pipe is of the common form, with square edges, as in Figs. 3 and 4, Table 2 gives the head for velocity direct. For very long pipes this is so small in proportion to the head due to friction, that it may in such cases be neglected, and we have omitted it for that reason in the preceding illustrations, thus, we found in (5) and in (6) that with 320 gallons, by an 8 inch pipe 3457 yards long, the head due to friction alone was 44.46 feet. By Table 2 it will be seen that the head for velocity at entry is rather less than 2 inches, so that in such a case it may be neglected. But when a pipe is very short, the head due to velocity may be much greater than that due to friction, and the most serious errors may be made by neglecting it. Say we had an 18-inch pipe, 20 yards long, discharging 3000 gallons. By Table 3 the friction is  $.0196 \times 20 = 392$  foot, and the head due to velocity by Table 2 is 6 inches, or 5 foot, being more than that due to friction, so that the total head is  $392 + 5 = .892$  foot.

(13) When, with a very short pipe, the head is given and the discharge has to be calculated, the case does not admit of a

simple direct solution, because we cannot tell beforehand in what proportions the total head at disposal has to be divided between overcoming friction and generating velocity. We must for such cases, apply a useful general law (27), which may be stated as follows — “*The discharge by any pipe or series of pipes, is proportional to the square root of the head,*” and conversely, “*The head is proportional to the square of the discharge,*” and these laws are true in pipes with bends jets, contractions, &c. Thus, say we require the discharge of a 12 inch pipe 5 yards long with 10 feet head. Assume a discharge, it is unimportant whether the assumed discharge is near the true quantity or not, or whether it is too much or too little. Say, in our case, we take it at 1000 gallons per minute, then by Table 3 the head for friction is  $01653 \times 5 = 08265$  foot, and the head for velocity is, by Table 2, about 4 inches, or 333 foot, making a total of  $08265 + 333 = 41565$  foot, instead of 10 feet, the head at disposal. Then applying the law just given, we have

$$\frac{1000 \times \sqrt{10}}{\sqrt{41565}} = \frac{1000 \times 3.162}{6147} = 4905 \text{ gallons}$$

Now, if in this case the head due to velocity had been neglected, the discharge by Table 3 would be  $\frac{10}{5} = 2.0 = 11,000$  gallons, which is more than double the true discharge. The Table 2 gives the greatest possible facility for making the calculations of head due to velocity, which should never be overlooked in cases where the pipe is short.

(14.) ”*Loss of Head by Bends* —There is another source of loss of head in pipes—namely, change of direction or bends. The best formula for calculating this loss is that of Weisbach, which may be modified into the following —

$$H = \left\{ 131 + (1.817 \times \left(\frac{r}{R}\right)^{\frac{2}{3}}) \right\} \times \frac{V^2 \times \phi}{960},$$

$$\text{and } V^2 = \frac{960 \times H}{\phi \times \left\{ 131 + (1.817 \times \left(\frac{r}{R}\right)^{\frac{2}{3}}) \right\}}.$$

In which  $H$  = the head due to change of direction, in inches

$r$  = radius of the bore of the pipe, in inches

$R$  = radius of the centre line of the bend, in inches

$\phi$  = angle of bend, in degrees.

$V$  = velocity of discharge, in feet per second

Thus, say we require the loss of head by a bend of 9 inches radius in a 6 inch pipe, discharging 800 gallons per minute, with an angle of  $55^\circ$ . A 6 inch pipe containing roughly  $\frac{6}{30} = 1\frac{1}{2}$

gallon per foot run the velocity of discharge will be  $\frac{800}{1\frac{1}{2} \times 60}$

$= 11\frac{1}{12}$  feet per second To find  $\left(\frac{r}{R}\right)^{\frac{1}{2}}$ , or in our case  $\left(\frac{3}{9}\right)^{\frac{1}{2}}$ ,

we have  $\frac{3}{9} = 3333$

Then the log of 3333 = 7.522835

7

2)4 659845

—————  
2 329922 = 02137 =  $\left(\frac{3}{9}\right)^{\frac{1}{2}}$

Then  $\left\{ 131 + (1.847 \times 02137) \right\} \times \frac{11\frac{1}{12} \times 55}{960} = 1\frac{1}{2}$  inch

the head required

Table 4 has been calculated by the second formula. The first part is adapted to bends of the radius usually met with in practice this may vary slightly with different makers but not so much as to affect the result seriously Fig 6 gives the proportions of the 8 inch bend as an illustration The second part of the Table gives the loss by *quick* bends of the proportions given by Fig 7, which are sometimes necessary in special cases they are commonly named elbows

Table 4 requires but little explanation, it shows for instance that an ordinary 8 inch bend with 18 inches radius consumes 3 inches head when passing 1970 gallons per minute, but a quick 8 inch bend with 6 inches radius consumes 12 inches

TABLE 4.—TABLE for Densities in WATER PIPE, showing the Loss of HEAD due to Change of Diameter by  
One Foot of Head.

**LOSS OR TRADE IN BENDS**

Diameter in Inches	Radius of Curve in feet											
	1	2	3	4	5	6	7	8	9	10	11	12
2	12	25	36	51	63	73	81	103	126	146	163	179
3	12	55	83	117	141	165	201	256	289	312	341	376
4	12	102	145	205	253	291	348	501	619	793	916	1041
5	18	102	229	321	399	448	501	650	803	928	1130	1312
6	18	232	328	461	568	650	744	10-0	1226	1514	1719	1914
7	18	309	437	618	757	874	10-0	1226	1514	1719	1914	2111
8	18	402	503	681	865	1137	1393	1608	1970	2271	2512	2763
9	18	501	701	1003	1255	1418	1737	2005	2365	2632	2890	3150
10	18	606	857	1225	1481	1711	2100	2411	2668	3166	4215	5160
11	21	868	1225	1723	2221	2551	3003	3166	3756	4276	4826	5370
12	21	1317	1861	2606	3714	5141	6563	8056	9503	11545	12870	14295
13	27	1857	2606	3714	5141	6563	8056	9503	11545	12870	14295	15508
14	27	2167	3190	4300	5635	7145	8650	10160	11700	13210	14730	16250
15	27	2167	3190	4300	5635	7145	8650	10160	11700	13210	14730	16250
16	30	2167	3190	4300	5635	7145	8650	10160	11700	13210	14730	16250

Table for Quick Review											
2	3	4	5	6	7	8	9	10	11	12	13
3	4	5	6	7	8	9	10	11	12	13	14
4	5	6	7	8	9	10	11	12	13	14	15
5	6	7	8	9	10	11	12	13	14	15	16
6	7	8	9	10	11	12	13	14	15	16	17
7	8	9	10	11	12	13	14	15	16	17	18
8	9	10	11	12	13	14	15	16	17	18	19

head when passing nearly the same quantity, or 1950 gallons, and these, it should be observed, are the heads due simply to change of direction, and do not include the head due to velocity or to friction. Thus, for instance, if the quick 8-inch bend had a length of one yard, the head for friction by Table 3 (say for 2000 gallons) would be 5 foot, and the head for velocity at entry by the rule in (3), namely  $\left(\frac{G}{d^2 \times 13}\right)^2 = H$  is  $\left(\frac{1950}{8^2 \times 13}\right)^2 = 5.48$  feet. Thus we have a total for such a bend of 1.0 foot for change of direction.

1 0 feet for change of direction,  
 0 5 " for friction,  
 5 48 " for velocity at entry,  
6 98 " total

Again, in a 6-inch pipe carrying 800 gallons, the Table shows that each common bend causes a loss of  $1\frac{1}{2}$  inches head, and each quick bend a loss of 5 inches, &c. The Table is arranged for bends of  $90^\circ$ , or quarter bends, as they are technically named, but it is applicable to any other angle, for the loss of head is simply proportional to the angle, the radius being the sum, thus, a half-quarter bend of  $45^\circ$ , or one-eighth part of a circle, consumes half the head of a bend of  $90^\circ$ , and a bend of  $180^\circ$ , or half a circle, takes double, &c., &c.

(15) "*Discharge of Compound Water mains*"—When a long main is composed of pipes of different sizes, as is very frequently the case, the head for each must be separately calculated, and the sum total taken. Thus, if we required 300 gallons per minute through a main 1200 yards long, composed of 800 yards of 7 inch, 300 yards of 6 inch, and 100 yards of 6 inch pipe, the head would be—

By Table 3.

$$\begin{array}{l}
 300 \text{ gallons } 7\text{-inch} = 022 \times 300 = 17 \text{ 6 feet head} \\
 " " 6 , = 0176 \times 300 = 14 \text{ 28 } " \\
 " " 5 " = 1185 \times 100 = 11 \text{ 85 } " \\
 \hline
 & & 43 \text{ 73 total}
 \end{array}$$

If there were bends in the pipes we must add the head for

them from Table 4, but it will be found, as in the case of head for velocity, see (12), that with long mains the effect of bends is very small. Say we had

4 common	bends in the 7-inch,	each $\frac{1}{8}$ -inch head	$= \frac{1}{2}$ inch
3 quick	" "	7 "	$\frac{1}{2}$ " $= 1\frac{1}{2}$ "
2 common	" "	6 "	$\frac{1}{4}$ " $= \frac{1}{2}$ "
2 quick	" "	6 "	$\frac{3}{4}$ " $= 1\frac{1}{2}$ "
4 common	" "	5 "	$\frac{1}{2}$ " $= 2$ "
3 quick	" "	5 "	$1\frac{1}{2}$ " $= 4\frac{1}{2}$ "
Total 10} inches			

Thus, even for such a large number of bends, the loss of head is only  $10\frac{1}{2}$  inches, or 875 of a foot, so that the total loss is  $43\frac{7}{8} + 875 = 44\frac{605}{8}$  feet.

(16) When, with such a series of pipes the head is given, and the discharge has to be determined, the case does not admit of a direct solution, because we cannot tell beforehand in what proportions the given head must be divided among the different pipes. We must in that case follow the course explained in (13) thus, say we required the discharge with 30 feet head by a main 2000 yards long, composed of 1200 yards of 8-inch pipe with four common bends in it, 700 yards of 6-inch pipe and three bends, and 100 yards of 5-inch pipe, with two common and two quick bends. The first thing to be done is to assume a discharge, and calculate the head for that, as was done in the last example, it is unimportant whether the assumed discharge is near the true quantity or not. Say in our case we take it at 400 gallons. Then

	By Table 3.	Length	Head
400 gallons 8-inch pipe	$= 02 \times 1200$	$= 24$	0 head
" 6 "	$= 085 \times 700$	$= 59$	5 "
" 5 "	$= 21 \times 100$	$= 21$	0 "
Carried forward			<u>101 5</u>

	Brought forward . 101 5 feet		
	Inch	Incl	In h
1 common bends in 8 each	$\frac{1}{8} \times 4 = \frac{1}{2}$	head	
3 " " "	6 "	$\frac{1}{2} \times 3 = 1\frac{1}{2}$	"
2 " " "	5 "	$\frac{1}{2} \times 2 = 1\frac{1}{2}$	"
2 quick " "	5 "	$3 \times 2 = 6$	"
			$9\frac{1}{2} = .8$ foot
			Total <u>105 3</u> feet

Thus we find that for 400 gallons we require 105 3 feet head instead of 30 feet, the head given, then by the rule in (13)

we have  $\frac{\sqrt{30 \times 100}}{\sqrt{105 3}}$  or  $\frac{5 447 \times 400}{10 26} = 213$  gallons, the real discharge sought. Further illustrations will be found in Chapter II.

(17) "*Effect of Contour of Section*"—The contour of the section of the line of pipes is a matter of some importance. The best condition, when the pipe is of uniform diameter from end to end, is, of course, a uniform slope throughout. This, however, can rarely be obtained, the pipe having to follow the contour of the ground, as in Fig 9. If a number of open topped pipes were inserted anywhere along the main, as at A, B, C, D, &c, the water would rise in them to the level of the oblique line J K, which in the case of a pipe of the same bore from end to end, would be a straight line as shown, this line is termed the *hydraulic mean gradient*. Now, the vertical distance from any point in that line (say the top of E) to the level line K M, will give the head for friction between E and K, and the vertical distance from the same point to the level line J L will give the friction between E and J. We have here supposed, of course, that the figure is correctly drawn to scale.

(18) When, as in Fig 11, the pipes are of different diameters, then each would have its own gradient, showing at every point the loss of head due to that particular pipe as in the figure. No loss of effect will arise from the pipe following the section of the ground, so long as the contour of the pipe does not anywhere along the line rise above the *hydraulic mean gradient*. Thus, in

Fig 9, where the ground is much broken, but does not anywhere rise above the gradient, the discharge will be the same as by a pipe with a uniform slope.

(19) But if, as in Fig 10, a hill, as at B, rises higher than the gradient, then the pipe from O to D will be in a state of partial vacuum, air will be given out by the water, and will accumulate at the summit, and being driven forward by the water from O to B, will remain permanently in the pipe from B to G, occupying the upper part of the pipe while the water trickles down the lower part as in a trough or open channel, and the vertical head from B to G is lost, the hydraulic gradient being now from A to B from B to G, and from G to F, this last being parallel to that from A to B, or at the same angle with the horizon. The discharge at F will therefore be, not the amount due to the head E, F on the length A, F, but that due to the head E, B on the length A, B.

(20) In this case the size of the pipe should not be uniform from end to end. From A to B it should be of large diameter, so as to deliver at B the required quantity with the head E, B, and the pipe from B to F may be of smaller diameter, so as to deliver the same quantity at F with the head H, F. Say we take a case with the length A, F = 5000 yards and head E, F = 90 feet, and that the length A, B = 2400 yards, and the head E, B = 10 feet, and that 500 gallons were required at F. With

uniform slope we should have  $\frac{90}{5000} = 018$ , which, by Table 3,

is a 9-inch pipe, or rather less for a 9-inch pipe would deliver 500 gallons with  $01742 \times 5000 = 87\frac{1}{2}$  feet. But for the delivery

at B with 10 feet head, and a 9 inch pipe, we have  $\frac{10}{2400} = 004167$ ,

which by Table = 24 $\frac{1}{2}$  gallons only, instead of 500, and, of course, this is all we should get at F with such an arrangement, for whatever the size of the rest of the pipe from B to F might be, it could not deliver more than it received by the pipe A, B.

The pipe from A to B should be  $\frac{10}{2400} = 004167$ , by Table 3

= a 12-inch pipe, and the pipe from B to F may be  $\frac{80}{2600} = .03077$  = an 8-inch pipe by Table. We may check these results thus —

	By Table 2.	Length	Head.
12-inch pipe, 560 gallons =	$00413 \times 2400 =$	9 912 feet	
8 " 500 "	$.0314 \times 2600 =$	81 64 "	
		Total 91 552	

Thus we find the exact head to be a little more than the head at disposal, but in most cases the agreement is near enough for practice.

(21) When a long main is composed of different sizes of pipes and passes over uneven ground the best course is to draw the gradients on the section of the pipes so as to see at a glance that none of the hill-tops rise above them. Fig 11 is a case in which, with a fall of 232 feet, we have a 10 inch main 1000 yards long, an 8-inch main 3000 yards long, and a 6-inch main 2000 yards long. To divide the given fall in the proper proportion between the different pipes and so find the gradients, let us assume that 100 gallons are delivered, then

	By Table 2. Length	A
100 gallons 10-inch =	$000411 \times 4000 =$	1 644 feet head
" 8 " =	$001256 \times 3000 =$	3 768 "
" 6 " =	$005292 \times 2000 =$	10 584 "
15 996 total head		

Now, whatever the real head may be, it would have to be divided among the several pipes in the same proportions as for 100 gallons in Col A, and as the head in our case is  $\frac{232}{15 996} = 14.504$  times the total head for 100 gallons, it follows that the real head for each pipe will be 14.504 times the head for the same pipe in Col A, thus the true head.

$$\begin{aligned}
 E, B \text{ for the 10 inch pipe will be } & 1 644 \times 14.504 = 23.44 \text{ feet} \\
 F, C \quad " \quad 8 " \quad " \quad & 3 768 \times 14.504 = 53.60 \text{ "} \\
 G, D \quad " \quad 6 " \quad " \quad & 10 584 \times 14.504 = 153.51 \text{ "} \\
 & \hline 232.00
 \end{aligned}$$

We can now draw the gradients on the section as in Fig 11, and then if the contour of the ground is below them throughout, all is well\*. The discharge at D may be calculated from any one of the pipes, say we take the 8-inch, then  $\frac{54.65}{3000} = 0.01822 =$  about 380 gallons by Table 3

(22) "*Special Cases*"—There are many cases for the solution of which no general rules can be given—they require reasoning, with the assistance of rules. The following cases may be useful—Say that with pipes, arranged as in Fig 12, we require 50 gallons at B, and 100 gallons at A, and have to determine the sizes of the mains. If we assume 3 inches for E, the head for that size would be  $0.423 \times 160 = 6.77$  feet above the level at B, and as that point is 8 feet (or 18 - 10) above the level at C, we have at this last point the head of  $6.77 + 8 = 14.77$  feet to deliver 50 gallons at B. Now, as A is  $25 - 18 = 7$  feet below C, the head on A will be  $11.77 + 7 = 21.77$  feet, and to find the size of pipe with that head for 100 gallons, we have  $\frac{21.77}{250} = 0.0871 =$  a 3½-inch pipe by Table 3

We have now only to fix the size of the pipe D to carry  $50 + 100 = 150$  gallons we find the head at C necessary for the pipes E and F to be 11.77 feet, leaving therefore only  $18 - 11.77 = 3.23$  feet for the friction of D and from this we find  $\frac{3.23}{300} = 0.01077 =$  a 6-inch pipe by Table 3

(23) Take another case shown by Fig 13 and say that we require the head at D to deliver 600 gallons at 1½ times the single and double line of pipes, also to find what proportion of the 600 gallons passes through two branches A, C, B at 1A, B. Let us assume that the pipe A, C, B carries 100 gallons, then the head at A for that quantity will be—

$$\begin{aligned} 1000 \text{ gallons } 12 \text{ inch } 1 \text{ in. } &= 0.167 \times 1100 = 18.38 \text{ feet head} \\ " 9 " &= 0.7 \times 8.38 = 5.86 " \\ & 7.1 " \end{aligned}$$

\* This principle has been tested in cases of great importance in the Army Corps of Engineers.

And with that head at A, the pipe A, B would at the same time deliver  $\frac{73.94}{950} = .0778 = 790$  gallons by Table 3; so that the two sets of pipes deliver at B 1790 gallons with a head of 73.94 feet at A, and therefore (13) to deliver the 600 gallons required would take  $\frac{73.94 \times 600}{1790} = 8.3$  feet. Then, the 12-inch pipe from D to A would require for 600 gallons  $.00595 \times 1100 = 6.545$  feet head, and the 9-inch pipe from B to E,  $.02509 \times 400 = 10.036$  feet; thus the total head at D will be  $6.545 + 8.3 + 10.036 = 24.881$  feet. The pipe A, C, B will carry  $\frac{600 \times 1000}{1790} = 336$  gallons, therefore the pipe A, B must take the rest, or 264 gallons.

(24.) If the head had been given, and the discharge due thereto had to be determined, we must have calculated the head for an assumed discharge, and then applied the rule in (13) to find the real discharge with the true head. Thus, say that with the same arrangement of pipes, we require the discharge at E with 45 feet head at D. If we assume 600 gallons, we should find 24.881 feet head as in (23); then  $\frac{600 \times \sqrt{45}}{\sqrt{24.881}}$  or  $\frac{600 \times 6.703}{4.988} = 807$  gallons, the discharge at E with 45 feet head at D, &c.

(25.) "*Delivery and Suction-pipes to Pumps.*"—In calculating the sizes of pipes to pumps, it should be remembered that the action of a pump is intermittent, especially where there is no air-vessel to equalize the velocity of supply and discharge. Say we have a single-acting pump 2 feet diameter and 2 feet stroke, worked by a crank, &c., making 16 revolutions per minute. The area of the pump being  $3.1416$  feet, we should have  $3.1416 \times 2 \times 16 = 100$  gallons discharged per minute; but while the bucket is descending the delivery is *nothing*, and it rises to a maximum when the bucket is at the centre of its up-stroke, where

it has the velocity of the crank pin, thus in our case the crank-path being 2 feet diameter, or 6 28 feet circumference, the maximum discharge at that moment is  $6 \frac{2}{7} \times 16 \times 3 = 1416$  = 314 gallons, and the pipes must be calculated for that quantity instead of 100 gallons, the mean discharge. In most cases, an air vessel is used, which more or less effectively regulates and equalizes the velocity of discharge. Where the suction-pipe is a long one, an air-vessel should be provided for that also. Table 5 gives the variation in velocity in different kinds of pumps without air vessels.

TABLE 5.—OF THE VELOCITY OF DISCHARGE BY PUMPS WITHOUT AIR VESSELS

	Velocity of Discharge			Var. in per cent.
	Max.	Mean	Min.	
One single-acting pump, worked by a crank	314 16	100	000	314 16
Two ditto, worked by cranks at right angles	222 00	100	000	222 00
One double-acting pump	157 08	100	000	157 08
Three-throw single-acting	101 76	100	90 63	14 07
Four single-acting or two double-acting	111 00	100	78 79	32 21

This Table shows that the common 3 throw pump has a more uniform discharge than any other, the maximum velocity being under 5 per cent in excess of the mean, an air-vessel is hardly necessary for such a case, in fact large pumps throwing 600 gallons per minute have been worked for many years successfully without any air-vessel.

(26) "Service-pipes in Towns"—The sizes of street service-pipes for town supplies cannot be calculated by the ordinary rules we may pursue another method. Certain sizes of lead services varying with the sizes of the houses supplied have been found necessary by experience. For ordinary cases with intermittent supply we may admit that  $\frac{1}{2}$ -inch pipe will suffice for a house with 6 or 7 rooms,  $\frac{3}{4}$  inch for 10 rooms,  $\frac{1}{2}$ -inch for 16 rooms, and 1-inch for say 30 rooms. The discharging power of long

pipes varies, as the  $2/5$  power of the diameter (28), thus  $4^{2/5} = 32$ , and we shall therefore require 32 1-inch pipes to deliver with the same head and length the same quantity of water as a 4-inch pipe, and we may admit that a 4-inch main would supply 32 1-inch lead services, &c. Table 6 is calculated on these principles.

TABLE 6.—SERVICE MAINS FOR WATER SUPPLY IN TOWNS

Diameter of Branch Mains	Diameter of Lead Services			
	$\frac{1}{2}$	$\frac{2}{3}$	$\frac{3}{4}$	1
Number of Houses supplied				
$1\frac{1}{2}$	15	9	6	3
2	32	18	12	6
$2\frac{1}{2}$	56	32	20	10
3	88	50	32	15
$3\frac{1}{2}$		74	47	23
4		104	66	32

"General Laws for Pipes"—The following general statement of the laws governing pipe questions may be useful; some of these laws apply strictly only to long mains in which the head due to velocity may be neglected.

(27) When  $d$  and  $L$  are constant, the discharge, or  $G$ , varies directly as the square root of the head, so that for heads in the ratio 1, 2, 3, the discharge would be in the ratio  $\sqrt{1}$ ,  $\sqrt{2}$ , and  $\sqrt{3}$ , or 1, 1.414, and 1.732.

Conversely,—the head is directly as the square of the discharge, so that for discharges in the ratio 1, 2, 3, we require heads in the ratio  $1^2$ ,  $2^2$ ,  $3^2$ , or 1, 4, 9, &c.

(28) When  $H$  and  $L$  are constant, the discharge is directly as the  $2/5$  power of the diameter, thus with diameters in the ratio 1, 2, 3, the discharge will be in the ratio  $1^{2/5}$ ,  $2^{2/5}$ , and  $3^{2/5}$ , or 1, 1.56, and 1.56.

Conversely,—the diameter will vary directly as the  $2/5$  root of the discharge, thus for discharges in the ratio 1, 2, 3, the

diameter will vary in the ratio  $\sqrt[3]{1}$ ,  $\sqrt[3]{2}$ , and  $\sqrt[3]{3}$ , or 1, 1.32, and 1.55, &c.

(29) When G and L are constant, the head will be inversely as the 5th power of the diameter, so that for diameters in the ratio 1, 2, 4, the heads will be in the ratio 1<sup>5</sup>, 2<sup>5</sup>, and 4<sup>5</sup>, or 1024, 32, and 1.

Conversely,—the diameter will be inversely as the 5th root of the head, thus for heads in the ratio 1, 2, 4, the diameters would be in the ratio  $\sqrt[5]{4}$ ,  $\sqrt[5]{2}$ , and  $\sqrt[5]{1}$ , or 1.32, 1.15, and 1.0, &c.

(30) When H and d are constant, the discharge will be inversely as the square root of the length, thus for lengths in the ratio 1, 2, 4, the discharge would be in the ratio  $\sqrt{4}$ ,  $\sqrt{2}$ , and  $\sqrt{1}$ , or 2.0, 1.414, and 1.0, &c.

Conversely,—the length varies inversely as the square of the discharge, thus for discharges in the ratio 1, 2, 4, the lengths would be in the ratio 4<sup>2</sup>, 2<sup>2</sup>, and 1<sup>2</sup>, or 16, 4, and 1, &c.

(31) When G and d are constant, the head is directly and simply as the length, thus for lengths in the ratio 1, 2, 3, the heads would also be in the ratio 1, 2, 3, &c.

(32) "Head for very Low Velocities"—Table 3 gives the greatest possible facility for the calculation of pipe questions, as may be seen by the examples we have given, and for all ordinary cases the results are correct, but for very small velocities with low heads say under one foot, &c., experiment has shown that the discharges are less than that Table would give and for such cases Prony's more difficult and laborious rule seems to give the most correct results. The following rule is based on that of Prony—

Let  $d$  = diameter of the pipe in inches

$H$  = head of water in inches

$L$  = length of pipe in feet.

$G$  = gallons per minute

Then

$$\left(16.353 \times \frac{H \times d}{L} + .00065\right)^{\frac{1}{3}} - .0816 \times d^2 \times 2.01 = G$$

Thus, say we required the discharge by a 12-inch pipe 3000 feet long with 36 inches head then

$$\left( 16 \cdot 353 \times \frac{36 \times 12}{3000} + 00665 \right)^{\frac{1}{2}} - .0816 \times 144 \times 2 \cdot 04 = 427 \text{ 4 gallons}$$

We may compare this result with that by Table 3, or rather by the rule  $\left( \frac{(3d)^3 \times H}{L} \right)^{\frac{1}{2}} = G$ , given in (5), by which the discharge comes out 426 gallons, or practically the same as by Prony's rule. With a very small head, however, the two rules do not agree, thus, with only one inch head, this same pipe gives 51.87 gallons by Prony's rule, whereas the other rule gives 70.98 gallons, or 29 per cent more. With a large head, on the contrary, Prony's rule gives a rather larger discharge than the other. The general comparison of the two rules may be shown by the case of a 10-inch pipe, 1000 yards long, the calculated discharge of which, with different heads, is given by the following Table —

	Head of Water						Discharge in Gallons per Minut.					
	in. 1	in. 4	ft. 1	ft. 4	ft. 5	ft. 4	ft. 21	ft. 4	ft. 85	ft. 4		
By the Rule in (5)	45	90	180	360	720	1110						
B; Prony's Rule	33.8	80.05	174.6	351.7	715	1107						
Difference per cent.	+33.1	+11.8	+3.1	-1.3	-3.41	-4.15						

(33) When the head is the unknown quantity, and the rest of the particulars are given, the rule becomes —

$$\left( \frac{G}{2 \cdot 01 \times d^3} + 0816 \right)^{\frac{1}{2}} - .00005 \times \frac{L}{d} = H$$

16.353

Let us take an extreme case, in order to illustrate more fully the special adaptation of Prony's formula to very low velocities

Say we require the head for a 10 inch pipe 4000 feet long, discharging only 20 gallons per minute then

$$\frac{\left(\frac{20}{2.04 \times 100} + 0.816\right)^2 - 0.00665}{16.353} \times \frac{4000}{10} = 626 \text{ inch head}$$

Now, by Table 3, the head comes out  $0.0001646 \times 1333 = 0.2194$  foot, or 263 inch only, so that in this very extreme case Prony's rule gives  $\frac{626}{263} = 2.38$  times the head by the rule in (5) or Table 3

(34) Table 29 has been calculated by the following modification of Prony's rule —

$$\frac{(V + 0.816)^2 - 0.00665}{196.24} = \frac{H \times d}{L},$$

In which  $d$  = diameter of pipe in inches

$V$  = velocity of discharge in feet per second.

$H$  = head of water in inches

$L$  = length of pipe in inches

Table 29 has been calculated for small velocities only, because Table 3 gives results sufficiently correct for practical purposes, with higher velocities and is more facile in application. We have added opposite each velocity in Table 29 the corresponding discharge of pipes from 1 inch to 24 inches diameter, in order to abridge the labour as much as possible. For the use of this Table we have the following rules —

(35) 1st To find the discharge, having  $H$ ,  $L$ , and  $d$  given. Multiply the given head in inches by the diameter in inches, and divide by the length in inches, and find the nearest number thereto in Col 1. Then opposite that number, and under the given diameter will be found the discharge in gallons per minute. Say, we take the case in (32) to find the discharge of a 12 inch pipe 3000 feet or 36,000 inches long with 36 inches head. Then  $\frac{H \times d}{L}$  or  $\frac{36 \times 12}{36000} = 0.12$ , the nearest number to which in

Col 1 is .01192, opposite to which, and under 12 inches diameter, is 427 gallons, the discharge sought

2nd To find the head, having G, L, and  $d$  given In Table 29, under the given diameter, find the nearest number of gallons, and take from Col 1 the number opposite to it, which number, multiplied by the length in inches, and divided by the diameter in inches, will give the required head in inches Thus, taking the extreme case in (33) to find the head for a 10 inch pipe 4000 feet long, with 20 gallons per minute —The nearest discharge under 10 inches diameter is 20.45 gallons, opposite which in Col 1 is .0001311, and from this we obtain  $\frac{.0001311 \times 48000}{10} =$

643 inch head the exact head for 20 gallons we calculated in (33) to be 626 inch

It should be observed that Prony's formula does not include the head due to velocity of entry (12), which for short pipes becomes important It has been omitted in the preceding illustrations because with such long pipes as were given in our cases it is too small to affect the result sensibly for instance, in the last case, the head for velocity with 20 gallons per minute and a 10-inch pipe by the rule in (3) is  $\left(\frac{20}{100 \times 13}\right)^2 = .000237$  foot, or  $\frac{1}{32}$ nd of an inch only

(36) "Square and Rectangular Pipes"—The case of square or rectangular pipes may be assimilated to that of round ones, and the head or discharge may then be calculated by the same rules and Tables that we have given for the latter The velocity of discharge, whatever may be the form of the pipe or channel, is proportional to the hydraulic radius (57) or the sectional area, divided by the circumference or perimeter in round pipes this is always equal to one-fourth of the diameter

Say we have a rectangular channel 3 ft  $\times$  1.5 feet, Fig 39, the area is 1.5 feet, the perimeter 9 feet, and the hydraulic radius  $\frac{4 \cdot 5}{9} = .5$  foot, which is the same as that of a round pipe  $.5 \times 4 = 2$  feet diameter Then to find the head for friction

with such a channel, say 100 yards long, discharging 270 cubic feet per minute, we have a velocity of  $\frac{270}{4 \cdot 5} = 60$  feet per minute, or 1 foot per second, which by Table 29 is equal to 1178 gallons per minute with a 21-inch pipe, and by Col 1 of the same Table  $\frac{H \times d}{L} = 005928$ , therefore  $H = \frac{005928 \times L}{d}$ , or in our case  $\frac{005928 \times (100 \times 36)}{24} = 889$  inch, the head required. We

might have obtained the head approximately by Table 3, say for 1200 gallons =  $000744 \times (100 \times 12) = 8928$  inch

We might also have calculated the head more directly by Table 30 — Opposite 5 the given hydraulic radius, the nearest velocity to that given, or 60 feet per minute, is 61 feet, which is under 15 inches fall per mile, or 00852 inch per yard, hence for 100 yards the head is  $00852 \times 100 = 852$  inch

The head for velocity at entry must be added to that for friction, and may be found by Table 15 thus, with a square edged inlet, the head for a velocity of 1 foot per second is given by Col C at  $\frac{1}{4}$ th of an inch, the total head is therefore  $889 + .25 = 1 \ 139$  inch

By the application of the same principles, the head, or discharge of a channel of any sectional form whatever may be determined.

(37) "*Effect of Corrosion or Rust in Pipes*" — The rules and Tables for calculating the discharge of pipes are adapted only to clean and even surfaces, such as are commonly met with in new cast-iron pipes. But some soft waters contain a great deal of oxygen, which rapidly decomposes iron, forming rust, which is deposited, not in an even layer, but in nodules or carbuncles

These retard the flow, not so much by the reduction of diameter as by the alteration of the character of the surface A notable case of this kind occurred at Torquay, where a main about 14 miles long, composed of 14,267 yards of 10-inch, 10,085 yards of 9 inch, and 170 yards of 8-inch pipe, delivered only 317 gallons per minute, with 465 feet head We may calculate the

discharge by the method explained in (13) — Assuming 1000 gallons, we have by Table 3 —

$$\begin{aligned} \text{Friction of 10-inch} &= 04115 \times 14267 = 587 \text{ 1 foot head} \\ " 9 " &= 0697 \times 10085 = 702 \frac{9}{10} " " \\ " 8 " &= 1256 \times 170 = \underline{21 \frac{3}{10}} " " \\ &\qquad\qquad\qquad 1311 \frac{3}{10} " \text{ total} \end{aligned}$$

And from this, the discharge with the real head is  $\frac{\sqrt{465} \times 1000}{\sqrt{1311 \frac{3}{10}}}$

or  $\frac{21 \frac{564}{1000} \times 1000}{36 \frac{21}{1000}} = 595$  gallons But by Froude's rule (32) the discharge comes out 616 gallons The experimental discharge was therefore only  $\frac{317}{616} = .51$  or 51 per cent of the theoretical, or in round numbers the discharge was that due to  $\frac{1}{3}$  of the head so that  $\frac{2}{3}$  of the head was lost in undue friction An ingenious scraper, suggested by the late Mr Appold, and worked by the pressure of the water, was passed through the entire length of the pipes, and subsequently an improved one by W Froude, Esq., was used with remarkable results, the discharge being increased to 564, and eventually, by repeated scraping, to 634 gallons, which is 18 gallons, or 3 per cent more than the theoretical quantity Errors of observation, or in the reputed sizes of the pipes, may account for the discrepancy

Dr Angus Smith's process, by which pipes are coated all over with a black enamel, seems to be an effective remedy against rusting, such pipes have been used with Torquay water for years without being affected The process is very cheap, being only about 5s per ton for medium pipes, it can be effectively applied only in the process of casting, while the pipes are new and hot With such a smooth surface as this process produces, the discharging power must be increased in a higher ratio than the cost, so that such pipes must really be more economical than any other

## CHAPTER II.

## ON FOUNTAINS, JETS, &amp;c.

(38) "*Height of Jets with given Head:*"—When water issues vertically from a nozzle, as at J in Fig. 5, it should theoretically attain the height of the head, and  $h$  should be equal to  $H$ , but it has been found by experiment that the height of the jet is always less than the head, a loss arising from the resistance of the air. The difference, or  $h'$ , is found to increase with the absolute height of the jet, and to diminish with an increase in the diameter. There are very few reliable experiments on this subject, and the laws indicated by those we have are very intricate. The best experiments we have are given in Table 7, and from them we find that  $h'$  increases nearly in the ratio of the square of the head, so that if we draw to scale the successive heights found by experiment, as in Fig. 14, we obtain a curve which approximates to a parabola. Thus, for a  $\frac{1}{2}$ -inch jet, as in the Figure, with 160 feet head, the jet would have attained the height  $H$ , or 160 feet, if there had been no resistance from the air, but it is found by experiment that it only reaches 80 feet as at D, therefore  $h' = 80$  feet is lost. Again, with 80 feet head the jet should have reached C = 80 feet, but the experimental height is only 60 feet, and, in that case,  $h = 20$  feet. Thus with heads in the ratio of 1, 2, the loss is in the ratio  $1^2, 2^2$ , or 1 to 4, being in fact 20 and 80 feet.

(39) Experiment also shows, that the head being constant,  $h'$  varies nearly in inverse ratio to the diameter of the jet, for instance, we have just seen that with 80 feet head on the  $\frac{1}{2}$ -inch jet, 20 feet head is lost. Then with a jet 1 inch diameter the loss would be about 10 feet, and the height attained 70 feet, but with a  $\frac{1}{4}$ -inch jet the loss would be about 40 feet, and the height attained 40 feet, &c. Thus we have the elements for calculating approximately the loss of head for any particular case, not perfectly agreeing, perhaps, with the true law, but the best

TABLE 7.—OF EXPERIMENTS on the HEIGHT of JETS with DIFFERENT HEADS

Diam. of Jet in Inches.	Head on the Jet in Feet.	Height of Jet in Feet.		Error	Loss of Height by Jet in Feet.		
		Experi- ment	Calcu- lated		Experi- ment	Calcu- lated	
2½	365	294	292	-2 0	81	83	Chatsworth
1½	61	61	60 1	-0 9	3	3 9	Witley Court
..	92	84	83 86	-0 14	8	8 14	..
..	115	103	102 9	-0 7	12	12 7	..
1	445	109	136 0	+27 0	336	309	Torquay.
4	46	48	41 2	-1 8	3	4 8	Witley Court
..	69	62	59 0	-3 0	7	10 0	..
..	92	77	74 4	-2 6	15	17 6	..
..	115	93	87 5	-5 5	22	27 5	..
..	141	98	99 6	+1 6	43	41 4	..
..	162	106	107 3	+1 3	56	54 7	..
4	15	14 25	14 44	+0 19	0 75	0 56	Weisbach
..	80	27 81	27 75	-0 06	2 19	2 25	..
..	45	89 42	89 94	+0 52	5 58	5 06	..
..	60	48 86	51 00	+2 64	11 04	9 00	..
4	15	14 01	14 00	+0 02	0 96	0 94	..
..	30	26 41	26 25	-0 19	3 56	3 75	..
..	45	36 18	36 56	+0 38	8 82	8 44	..
..	60	42 96	45 00	+2 04	17 04	15 00	..
..	52	27	27 7	+0 7	5	4 3	Witley Court
..	46	86	37 2	+1 2	10	8 8	..
..	95	55	57 4	+2 4	40	37 6	..
..	118	63	60 0	-3 0	55	56 0	..
4	28 8	19	21 9	+2 9	9 8	6 9	..
..	64	30	30 0	0 0	34 0	31 0	..

approximation we can obtain this is a subject on which more experimental information is very desirable. Table 8 gives the height of jets with different heads, and is calculated by the following rule—

$$h' = \frac{H^2}{d} \times .0125;$$

In which  $H$  = the head on the jet in feet.

“  $h'$  = the difference between the height of head and height of jet

“  $d$  = diameter of jet in  $\frac{1}{8}$ ths of an inch.

TABLE 8.—Of the HEIGHT of JETS with DIFFERENT HEADS.

Head on Jet in Feet.	DIAMETER OF JET IN INCHES.											
	$\frac{1}{4}$	$\frac{1}{2}$	$\frac{3}{4}$	$\frac{1}{4}$	$\frac{5}{8}$	$\frac{3}{4}$	1	$1\frac{1}{4}$	$1\frac{1}{2}$	$1\frac{3}{4}$	2	
	HEIGHT OF JET IN FEET											
10	8.75	9.37	9.6	9.7	9.75	9.8	9.84	9.875	9.9	9.91	9.92	
20	15.0	17.5	18.33	18.75	19.0	19.2	19.4	19.5	19.6	19.6	19.7	
30	19.0	21.4	26.25	27.2	27.75	28.3	28.6	29.0	29.1	29.2	29.3	
40	20.0	30.0	33.3	35.0	36.0	37.0	37.5	38.0	38.3	38.6	38.7	
50	..	31.4	30.6	42.2	44.0	45.0	46.1	47.0	47.4	47.8	48.0	
60	..	37.5	45.0	48.7	51.0	52.0	54.4	55.0	56.2	56.6	57.0	
70	..	39.0	50.0	55.0	58.0	60.0	62.4	64.0	65.0	65.6	66.0	
80	..	40.0	53.0	60.0	64.0	67.0	70.0	72.0	73.8	74.2	75.0	
90	..	..	56.0	65.0	70.0	73.0	77.0	80.0	81.6	83.0	84.0	
100	..	..	58.0	69	75	79	81	87	90	91	92	
120	..	..	60.0	75	84	90	97	102	105	107	109	
140	..	..	..	79	91	99	109	116	120	123	125	
160	..	..	..	80	96	106	120	128	133	137	140	
180	..	..	..	..	99	112	129	139	141	151	155	
200	..	..	..	..	100	116	137	150	158	166	169	
220	..	..	..	..	..	119	145	159	165	177	182	
240	..	..	..	..	..	120	150	169	180	189	195	
260	..	..	..	..	..	..	155	175	190	200	208	
280	..	..	..	..	..	..	158	182	198	210	219	
300	..	..	..	..	..	..	160	187	206	220	230	
350	..	..	..	..	..	..	..	193	222	241	255	
400	..	..	..	..	..	..	..	200	233	257	275	

(40.) It is a result of this rule, that each particular size of jet attains its maximum height with a certain head, and that if the head is increased beyond that point, the height of jet is not increased thereby, but is actually diminished. This result is anomalous: it may be that an excessive head breaks the issuing stream into spray and causes it to meet with more resistance from the air than a jet of solid water issuing with a moderate head. Experiments with excessive heads show an enormous loss: thus a jet 1 inch diameter with 445 feet head, reached a height of about 109 feet only, as measured by a theodolite.

Our rule gives the loss  $k' = \frac{445^2}{8} \times .0125$ , or  $\frac{198025}{8} \times .0125$

TABLE 7.—OF EXPERIMENTS on the HEIGHT of JETS with DIFFERENT HEADS

Diam. of Jet in Inches.	Head on the Jet in Feet.	Height of Jet in Feet.		Error	Loss of Height by Jet in Feet.		
		Experi- ment	Calcu- lated		Experi- ment	Calcu- lated	
2½	365	284	282	-2 0	81	83	Chatsworth
1½	64	61	60 1	-0 9	3	3 9	Witley Court
..	92	84	83 86	-0 14	8	8 14	..
..	115	103	102 3	-0 7	12	12 7	..
1	445	109	136 0	+27 0	336	309	Torquay
¾	46	43	41 9	-1 8	3	4 8	Witley Court
..	69	62	59 0	-3 0	7	10 0	..
..	92	77	74 4	-2 6	15	17 6	..
..	115	93	87 5	-5 5	22	27 5	..
..	141	98	99 6	+1 6	43	41 4	..
.	162	106	107 3	+1 3	58	54 7	..
½	15	14 25	14 44	+0 19	0 75	0 58	Weisbach
..	30	27 81	27 75	-0 06	2 19	2 25	..
..	45	39 42	39 94	+0 52	5 58	5 08	..
..	60	48 36	51 00	+2 64	11 64	9 00	..
¾	15	14 04	14 06	+0 02	0 96	0 91	..
..	30	26 44	20 25	-0 19	3 56	3 75	..
..	45	38 18	36 56	+0 38	8 82	8 41	..
..	60	42 96	45 00	+2 04	17 04	15 00	..
..	92	27	27 7	+0 7	5	4 9	Witley Court
.	46	36	37 2	+1 2	10	8 8	..
..	95	55	57 4	+2 4	40	37 6	..
..	118	63	60 0	-3 0	55	58 0	..
½	28 8	19	21 9	+2 9	9 8	6 9	..
..	64	30	30 0	0 0	34 0	34 0	..

approximation we can obtain. This is a subject on which more experimental information is very desirable. Table 8 gives the height of jets with different heads, and is calculated by the following rule —

$$h' = \frac{H^2}{d} \times .0125;$$

In which  $H$  = the head on the jet in feet

“  $h'$  = the difference between the height of head and height of jet

“  $d$  = diameter of jet in  $\frac{1}{8}$ ths of an inch

TABLE 8.—Of the HEIGHT of JETS with DIFFERENT HEADS

Head on Jet in Feet.	DIAMETER OF JET IN INCHES.										
	$\frac{1}{2}$	$\frac{3}{4}$	$\frac{5}{8}$	$\frac{3}{5}$	$\frac{1}{2}$	$\frac{3}{4}$	1	$1\frac{1}{2}$	$1\frac{3}{4}$	$2\frac{1}{2}$	$2\frac{3}{4}$
	HEIGHT OF JET IN FEET										
10	8.75	9.37	9.6	9.7	9.75	9.8	9.81	9.875	9.9	9.91	9.92
20	15.0	17.5	18.3	18.75	19.0	19.2	19.4	19.5	19.6	19.6	19.7
30	19.0	24.4	26.2	25.2	27.75	29.3	28.6	29.0	29.1	29.2	29.3
40	20.0	30.0	33.3	35.0	36.0	37.0	37.5	38.0	38.3	38.6	38.7
50	31.4	39.6	42.2	41.0	45.0	46.1	47.0	47.4	47.8	48.0	
60		37.5	45.0	48.7	51.0	52.0	51.4	55.0	56.2	56.6	57.0
70		39.0	50.0	55.0	59.0	60.0	62.4	64.0	65.0	65.6	66.0
80		40.0	53.0	60.0	61.0	67.0	70.0	72.0	73.3	74.2	75.0
90			56.0	65.0	70.0	73.0	77.0	80.0	81.6	83.0	84.0
100			58.0	69.0	75	79	81	87	90	91	92
120		60.0	75	84	90	97	102	105	107	109	
140			79	91	99	109	116	120	123	125	
160			80	90	106	120	128	133	137	140	
180				99	112	129	139	141	151	155	
200	..			100	116	137	150	158	160	163	
220					119	145	159	163	177	182	
240					120	150	168	180	183	195	
260						155	175	190	200	204	
280						158	182	198	210	210	
300						160	187	206	210	210	
350							198	212	211	215	
400							200	233	237	235	

(40) It is a result of this rule, that each particular size of jet attains its maximum height with a certain head, and that if the head is increased beyond that point, the height of jet is not increased thereby, but is actually diminished. This result is anomalous—it may be that an excessive head breaks the flowing stream into spray and causes it to meet with more resistance from the air than a jet of such water leaving with a moderate head. Experiments with excessive heads show an effect no less than a jet 1 inch diameter with 445 feet head, reaches a height of about 103 feet only, as measured by a thread 103 ft.

$$\text{Our rule gives the loss } h = \frac{447^2}{g} \times 0.12^2, \text{ or } \frac{1000000}{g} \times 0.0144$$

= 309 feet, and hence the height of jet is  $445 - 309 = 136$  feet  
 The error of 27 feet is considerable, but perhaps not more than  
 might be expected in such an extreme case.

(41) "Discharge of Jets"—The quantity of water discharged  
 will vary considerably with the form of the nozzle. The form  
 is also a matter of importance, as affecting the solidity of the  
 issuing stream, and thereby the height of the jet. Fig 15 shows  
 the best form of nozzle, and Table 9 gives the general proportions

TABLE 9.—Of the PROPORTIONS of NOZZLES for JETS

	B	C	D.
in.	in.	in.	in.
45	6	3	
67	9	45	
90	12	6	
1 12	15	75	
1 33	18	9	
1 80	24	1 2	
2 23	30	1 5	
2 70	36	1 8	
3 15	42	2 1	
3 6	48	2 4	
4 0	54	2 7	
4 5	60	3 0	
4 9	66	3 3	
5 4	72	3 6	

for different sizes. The lip at E projecting beyond the mouth  
 is intended to protect the bore from indentation by accident.  
 The discharge by well made nozzles of this form will be about  
 913, the theoretical discharge being 1 0, and may be found  
 direct by the following rule —

$$G = \sqrt{H} \times d^2 \times 21,$$

In which H = the head of water on the jet in feet.

d = the diameter in  $\frac{1}{8}$ ths of an inch.

G = gallons discharged per minute.

Table 10 has been calculated by this rule.

(42) "Jets at the End of Long Mains"—When a jet is placed  
 at the end of a pipe, or series of pipes, as is usually the case,

FIG. 10.—Of the Discharge of Jets with Different Heads.

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
	GALLONS DISCHARGED PER MINUTE.																							
	FEET OF JET IN LENGTH.																							
1	6.55	8.59	13.4	19.3	26.3	31.4	36.3	41.3	46.1	51.1	56.1	61.1	66.1	71.1	76.1	81.1	86.1	91.1	96.1	101.1	106.1	111.1	116.1	
2	9.79	12.1	18.9	27.3	37.1	45.5	53.4	61.6	69.6	77.1	84.2	91.2	98.2	105.2	112.2	119.2	126.2	133.2	140.2	147.2	154.2	161.2	168.2	175.2
3	11.1	14.8	23.5	33.6	43.4	52.6	61.6	70.6	79.9	89.1	98.2	107.1	116.1	125.1	134.1	143.1	152.1	161.1	170.1	179.1	188.1	197.1	206.1	215.1
4	13.0	17.0	29.0	43.2	58.3	76.8	92.9	112.0	131.1	151.2	173.2	192.2	211.2	230.2	249.2	268.2	287.2	306.2	325.2	344.2	363.2	382.2	401.2	420.2
5	14.7	19.8	32.9	47.3	61.4	81.1	101.1	121.1	141.2	161.2	181.2	201.2	221.2	241.2	261.2	281.2	301.2	321.2	341.2	361.2	381.2	401.2	421.2	441.2
6	16.1	21.0	36.9	51.6	67.6	87.1	103.1	123.1	143.1	163.1	183.1	203.1	223.1	243.1	263.1	283.1	303.1	323.1	343.1	363.1	383.1	403.1	423.1	443.1
7	17.5	23.0	39.5	55.1	71.6	87.3	103.1	123.1	143.1	163.1	183.1	203.1	223.1	243.1	263.1	283.1	303.1	323.1	343.1	363.1	383.1	403.1	423.1	443.1
8	19.2	26.0	42.0	58.0	74.0	90.7	106.7	122.7	138.7	154.7	170.7	186.7	202.7	218.7	234.7	250.7	266.7	282.7	298.7	314.7	330.7	346.7	362.7	378.7
9	21.0	28.0	45.0	61.0	77.0	93.0	109.0	125.0	141.0	157.0	173.0	189.0	205.0	221.0	237.0	253.0	269.0	285.0	301.0	317.0	333.0	349.0	365.0	381.0
10	22.7	30.0	47.0	63.0	79.0	95.0	111.0	127.0	143.0	159.0	175.0	191.0	207.0	223.0	239.0	255.0	271.0	287.0	303.0	319.0	335.0	351.0	367.0	383.0
11	24.2	31.0	48.0	64.0	80.0	96.0	112.0	128.0	144.0	160.0	176.0	192.0	208.0	224.0	240.0	256.0	272.0	288.0	304.0	320.0	336.0	352.0	368.0	384.0
12	25.7	32.0	49.0	65.0	81.0	97.0	113.0	129.0	145.0	161.0	177.0	193.0	209.0	225.0	241.0	257.0	273.0	289.0	305.0	321.0	337.0	353.0	369.0	385.0
13	27.2	33.0	50.0	66.0	82.0	98.0	114.0	130.0	146.0	162.0	178.0	194.0	210.0	226.0	242.0	258.0	274.0	290.0	306.0	322.0	338.0	354.0	370.0	386.0
14	28.7	34.0	51.0	67.0	83.0	100.0	116.0	132.0	148.0	164.0	180.0	196.0	212.0	228.0	244.0	260.0	276.0	292.0	308.0	324.0	340.0	356.0	372.0	388.0
15	30.2	35.0	52.0	68.0	84.0	101.0	117.0	133.0	149.0	165.0	181.0	197.0	213.0	229.0	245.0	261.0	277.0	293.0	309.0	325.0	341.0	357.0	373.0	389.0
16	31.7	36.0	53.0	69.0	85.0	102.0	118.0	134.0	150.0	166.0	182.0	198.0	214.0	230.0	246.0	262.0	278.0	294.0	310.0	326.0	342.0	358.0	374.0	390.0
17	33.2	37.0	54.0	70.0	86.0	103.0	120.0	136.0	152.0	168.0	184.0	200.0	216.0	232.0	248.0	264.0	280.0	296.0	312.0	328.0	344.0	360.0	376.0	392.0
18	34.7	38.0	55.0	71.0	87.0	104.0	121.0	137.0	153.0	169.0	185.0	201.0	217.0	233.0	249.0	265.0	281.0	297.0	313.0	329.0	345.0	361.0	377.0	393.0
19	36.2	39.0	56.0	72.0	88.0	105.0	122.0	138.0	154.0	170.0	186.0	192.0	208.0	224.0	240.0	256.0	272.0	288.0	304.0	320.0	336.0	352.0	368.0	384.0
20	37.7	40.0	57.0	73.0	89.0	106.0	123.0	140.0	156.0	172.0	188.0	204.0	220.0	236.0	252.0	268.0	284.0	298.0	314.0	330.0	346.0	362.0	378.0	394.0
21	39.2	41.0	58.0	74.0	90.0	107.0	124.0	141.0	158.0	174.0	190.0	207.0	223.0	240.0	256.0	273.0	289.0	305.0	321.0	337.0	353.0	369.0	385.0	391.0
22	40.7	42.0	59.0	75.0	91.0	108.0	125.0	142.0	160.0	176.0	192.0	209.0	225.0	242.0	258.0	275.0	291.0	307.0	323.0	339.0	355.0	371.0	387.0	393.0
23	42.2	43.0	60.0	76.0	92.0	109.0	126.0	143.0	161.0	177.0	193.0	210.0	226.0	243.0	260.0	276.0	293.0	309.0	325.0	341.0	357.0	373.0	389.0	395.0
24	43.7	44.0	61.0	77.0	93.0	110.0	127.0	144.0	162.0	178.0	194.0	211.0	227.0	244.0	261.0	277.0	294.0	310.0	326.0	342.0	358.0	374.0	390.0	396.0

calculation must be made of the loss of head by friction in such pipes, so as to obtain the actual head on the jet, for which alone the rules and Table apply. Say, for illustration, we take the case, shown by Fig. 16, of a jet 1 inch diameter, 70 feet high, at the end of a long main 6 inches, 5 inches, and 4 inches diameter, of the respective lengths given by the Figure, and that we have to calculate the head necessary. Table 8 shows that a jet 1 inch diameter, 70 feet high, requires 80 feet head, and Table 10 gives the discharge of the same jet, with 80 feet head, at 137 gallons. Then, by Table 3, we calculate the friction of the mains, and we have the following results —

	Feet.
Head to play 1 inch jet 70 feet high	= 80 00
Friction 6 inch main, say 140 gallons = $01037 \times 800 =$	6 22
" 5 " " = $078 \times 800 =$	7 74
" 4 " " = $0788 \times 100 =$	7 88
Total = 101 84	

(43) In other cases we may have the head and diameter of pipes and nozzle given, and have to determine the discharge. This case is illustrated by Fig. 17, and in dealing with it, we must follow the course indicated in (13). Say we assume the discharge at 300 gallons, Table 10 shows that a jet  $1\frac{1}{2}$  inch diameter requires about 75 feet head for that quantity. Then, by Table 3, we find the friction of the mains as follows —

	Feet.
Head to play $1\frac{1}{2}$ inch jet 300 gallons	= 75 00
Friction 7 inch main, 300 gallons = $022 \times 800 =$	17 60
" 6 " " = $0476 \times 800 =$	19 04
" 5 " " = $1185 \times 80 =$	9 48
Total = 121 12	

So that for our assumed discharge of 300 gallons we require only 121 12 feet, instead of 150, the head at disposal. Then by the rule to (13) the true discharge with 150 feet head will be  $\frac{300 \times \sqrt{150}}{\sqrt{121 12}} = 334$  gallons. In such cases as this, where the height of a jet is involved, the discharge assumed should be pretty near the true one.

(44) In another case we might require to find the diameter of one of the main pipes, having all the rest given. Thus, say that we have to find the diameter of the pipe P, in Fig. 18. Table 8 gives 90 feet as the head for  $1\frac{1}{2}$  jet 80 feet high, and Table 10 gives 227 gallons as the discharge of the same jet with 90 feet head.

Then, $1\frac{1}{2}$ jet 80 feet high, by Table 8	90 0 feet head
Friction of 6 inch main = $028 \times 400$	$\frac{11}{11} 2$ "
	$\underline{101} \ 2$ "

We have therefore  $115 - 101 2 = 13 8$  feet of head left for the friction of the pipe P, or  $\frac{13}{200} 8 = 069$  foot per yard, which by Table 3 is equal to a 5 inch pipe with say 230 gallons, and this is the required diameter of the pipe P.

(45) *Path of Fountain Jets* —When the discharge takes place obliquely, or out of the perpendicular, the path of the jet is a parabola, and may be conveniently described by the method shown in Fig. 23, in which we have a jet discharging upward at an angle of  $45^\circ$ , and with a head of 14 feet which by Table 11 will give a velocity of 30 feet per second, or 8 feet per tenth of a second. If we mark on the line S, E a series of points A, B, C, &c., 3 feet apart, they would show the position of a particle of water at each tenth of a second if gravity did not act—but of course gravity does act simultaneously, and Table 12 gives the space fallen through each tenth of a second, which being plotted on the perpendiculars drawn through each of the points A, B, C &c., will give the true position of the particle of water at each tenth of a second. Thus in  $\frac{1}{10}$ ths of a second it would have arrived at C, if uninfluenced by gravity, but the Table shows that in that time a body falls 1 foot  $5\frac{1}{2}$  inches, therefore F is the true position at that moment, and so of the rest, as in the Figure, which gives the path for two seconds. The lower curve S, T in Fig. 23, shows the path of a jet with the same head and velocity projected downwards at the same angle of  $45^\circ$ . Fig. 19 gives the path for a horizontal projection, and also

## FOUNTAINS--TABLES OF VELOCITIES.

TABLE 11.—FALLING BODIES, giving the SPACE fallen through to acquire certain VELOCITIES.

Velocity in Feet per Second.	Space.		Velocity in Feet per Second	Space.		Velocity in Feet per Second.	Space.	
1	ft.	ins.	21	ft.	10	41	ft.	1
2	0	0 $\frac{1}{2}$	22	7	6	42	27	5
3	0	1 $\frac{1}{2}$	23	8	3	43	28	9
4	0	3	24	9	0	44	30	1
5	0	4 $\frac{1}{2}$	25	9	9	45	31	5
6	0	6 $\frac{1}{2}$	26	10	6	46	32	10
7	0	9 $\frac{1}{2}$	27	11	4	47	34	4
8	1	0	28	12	3	48	36	10
9	1	3 $\frac{1}{2}$	29	13	0	49	37	4
10	1	6 $\frac{1}{2}$	30	14	0	50	38	11
11	1	10 $\frac{1}{2}$	31	14	11	52	42	0
12	2	0	32	15	11	54	45	4
13	2	7 $\frac{1}{2}$	33	16	11	56	50	0
14	3	0 $\frac{1}{2}$	34	18	0	58	52	0
15	3	6	35	19	0	60	50	0
16	4	0	36	20	1	62	59	8
17	4	0	37	21	5	64	63	8
18	5	0	38	22	6	66	67	8
19	5	7	39	23	9	68	72	0
20	6	3	40	24	11	70	76	0

TABLE 12.—FALLING BODIES

Time Seconds.	Whole Space fallen	Velocity acquired, Feet per Second	Time. Seconds.	Whole Space fallen.	Velocity acquired, Feet per Second.
$\frac{1}{2}$	ft. ins.	ft.	$\frac{1}{2}$	ft. ins.	ft.
$\frac{1}{2}$	0 1 $\frac{1}{2}$	3 2	$\frac{1}{2}$	19 4 $\frac{1}{2}$	35 2
$\frac{1}{2}$	0 7 $\frac{1}{2}$	6 4	$\frac{1}{2}$	23 0 $\frac{1}{2}$	38 4
$\frac{1}{2}$	1 5 $\frac{1}{2}$	9 6	$\frac{1}{2}$	27 0 $\frac{1}{2}$	41 6
$\frac{1}{2}$	2 6 $\frac{1}{2}$	12 8	$\frac{1}{2}$	31 *	41 8
$\frac{1}{2}$	4 0	16 0	$\frac{1}{2}$	*	48 0
$\frac{1}{2}$	5 9 $\frac{1}{2}$	19 2	$\frac{1}{2}$	*	51 2
$\frac{1}{2}$	7 10	22 4	$\frac{1}{2}$	*	54 4
$\frac{1}{2}$	10 2 $\frac{1}{2}$	25 6	$\frac{1}{2}$	*	57 4
$\frac{1}{2}$	12 11 $\frac{1}{2}$	28 8	$\frac{1}{2}$	*	
1	16 0	32 0	2		

illustrates another method of drawing the parabolic curve, which consists in dividing the total space filled through J, K into the same number of equal parts as the line H, J, and drawing radial lines from the point H, as shown. The path of the jet is through the intersections of the radial lines with the perpendiculars, as in the figure. The two methods give the same result precisely.

(46) There are some general laws governing the parabolic paths of jets which it will be well to state explicitly. Let Fig. 20 be a jet playing obliquely from a nozzle at J, and striking the horizontal plane at G.

1st If the line of direction of the pipe or axis of the jet be prolonged, it cuts the axis of the parabola at a point C, whose distance from the base is always double the height of the parabola, or CN is equal to twice DN. This gives a useful rule for finding the proper angle of the jet pipe when the path of the jet has been determined.

2nd If we find the focus of the parabola by the ordinary method, namely, by bisecting the radius of the base at A, drawing the line AD, and making AL perpendicular to AD, then the point L is the focus of the parabola and the distance NL is the extra head  $h$  necessary to play the jet horizontally, or the difference between the maximum height of the jet and the head upon it at J. Thus the total head H may be considered as divided into two portions, namely, H, which is equal to the height of the parabola DN, and  $h$ , which is equal to the distance of the focus of the parabola from the base.

3rd If, therefore, with the same head the jet were made to play vertically, it would (theoretically) attain the height of H, instead of H.

4th In all cases,  $h$  bears a certain proportion to the height of the parabola (H), and to the length of its base B, and may be calculated from those particulars by the rule  $h = \frac{(\frac{1}{2}B)^2}{H}$ , thus, to play a jet 32 feet horizontally (B), and 16 feet high (H), as in Fig. 21, we shall have  $h = \frac{8^2}{16} = 4$  feet, which, added to the

height of the jet path (16 feet), gives 20 feet for the total head on the jet

5th The horizontal distance from the nozzle at J to the point on the plane at G, where the jet strikes it, may be calculated when the total head H and the height of the parabola H are given, for obviously  $H - H = h$ , and knowing h, we may find B by the rule  $\sqrt{h} \times H \times 4 = B$ . Thus, in Fig 21, we have  $H' = 20$ , and  $H = 16$ , therefore,  $h = 20 - 16 = 4$ , and then  $\sqrt{4} \times 16 \times 4 = 32$  feet

6th When the jet issues horizontally, as in Fig 25, its path is half a parabola, following the same laws as before, namely,  $h = F$ , also  $h = \frac{(4P)^2}{H}$ , and  $\sqrt{h} \times H \times 2 = P$ , &c

(47) In some cases, the two half parabolas are unequal, as in Fig 24, where we have a jet 20 feet high at its maximum, delivering at N = 15 feet high, and 24 feet distant horizontally from the nozzle at J, and we require to find  $h$  = the extra head, and to describe the path of the jet. Here we have first to find the position of the centre line dividing the semi-parabolas, and to do this we have  $\frac{D \times \sqrt{H}}{\sqrt{H} + \sqrt{H}} = R$ , which

in our case becomes  $\frac{24 \times 4}{4 + 2} = \frac{472}{472 + 236} = 16$  feet. Then the focus of the two semi parabolas may be found as before, and it will be

found that F and F' are equal. Thus, in our case  $F = \frac{\left(\frac{16}{2}\right)^2}{20} =$

$\frac{\left(\frac{8}{2}\right)^2}{5} = 3\frac{2}{5}$  feet and  $F = 3\frac{2}{5}$  feet also. F being equal to h, we thns find h to be 3 2 feet, and the total head at J will therefore be  $20 + 3\frac{2}{5} = 23\frac{2}{5}$  feet (H). If we reverse the direction of the jet, placing the nozzle at N, instead of at J, then, with a head of  $5 + 3\frac{2}{5} = 8\frac{2}{5}$  feet, the path of the jet would be the same as before.

(48) We have followed throughout the investigation of the paths of oblique jets, the theoretical law that the height of the jet is equal to the head, and we have done this to avoid complicating the matter unnecessarily; but obviously, we must apply to oblique jets the correction we found necessary for perpendicular ones. Thus, if we had a jet  $\frac{1}{2}$ -inch diameter, with 80 feet head, Table 8 shows that the height attained vertically would be only 60 feet, and if this jet played obliquely, its path should be calculated for the latter height, but the quantity of water expended, and the value of  $h$  must be calculated for 80 feet.

Oblique jets of great height and range, deviate considerably from the true parabolic path assigned by the rules, the curve becomes in such cases like A, D, E in Fig 22, the true parabolic path being A, B, C. But for moderate heights and ranges, such as usually occur in practice, the deviation is not considerable.

(49) "*Ornamental Jets*"—There are many kinds of ornamental jets which may be used with pleasing effect in very sheltered situations, especially in the interior of conservatories, &c. One of these, called the "Convolvulus," from the form of its display, is shown in half-size section by Fig 26. The pressure of a very small head of water (2 or 3 feet) raises the valve B, and allows a thin sheet of water to escape, forming a sheet jet of the form given in Fig 27, and (with the size given by Fig 26) about 3 feet diameter, with an expenditure of about 6 gallons per minute.

Fig 28 is a half-size section of the "Dome" or "Globe" jet, which produces a display of the form shown by Fig 29, with a head of about 2 feet, the globe being about 14 inches diameter, and the expenditure about 3 gallons per minute. With a greater head say 3 or 4 feet, the display has the form of an umbrella about 21 inches diameter, expending about 4 gallons per minute.

The "Basket and Ball" jet is another pleasing variety, the basket is of fancy wire-work, large enough to catch the ball when it escapes from the jet of water, and formed so as to return it back to its place. The ball is formed of light wood (lime-tree is the best), painted or gilded, and well varnished.

There should be a certain proportion between the size of the ball and the diameter of the jet. As an approximation we may give the following rule —

$$\sqrt{d^2 \times 13} = D,$$

In which  $d$  = the diameter of the jet in  $\frac{1}{8}$ ths of an inch.

$D$  = the diameter of the ball in inches.

Table 13 has been calculated by this rule, it gives the proportions up to 1-inch jets, but the  $\frac{3}{4}$ -inch jet, with  $3\frac{1}{2}$ -inch ball is usually the maximum size in practice

TABLE 13 —For BALL JETS

Diameter of Jet	=	Diameter of Ball
$\frac{1}{8}$ -inch	=	$1\frac{1}{2}$ -inch
$\frac{1}{4}$ "	=	$1\frac{3}{4}$ "
$\frac{3}{8}$ "	=	$2\frac{1}{4}$ "
$\frac{1}{2}$ "	=	$2\frac{3}{4}$ "
$\frac{5}{8}$ "	=	$3\frac{1}{4}$ "
$\frac{3}{4}$ "	=	$3\frac{1}{2}$ "
$\frac{7}{8}$ "	=	4 "
1 "	=	$4\frac{1}{2}$ "

## CHAPTER III.

### ON CANALS, CULVERTS, AND WATER-COURSES

(70) "Open Water-courses"—The discharge of open water-courses may be found experimentally by observing the velocity of the current and measuring the cross sectional area of the stream. But to do this correctly we require the mean velocity throughout the section, which is not given by observation. The velocity varies, being a maximum at the surface and where the channel is deepest, which is usually near the centre of the width, diminishing from thence to the banks on either side, and to the bottom, where it is a minimum.

The best experiments we have, give the mean velocity

throughout the section at 81 per cent. of the maximum central surface velocity, which is usually the velocity observed, being easily obtained by a float on the surface of the stream (68). Table 14 gives the mean velocity corresponding to observed maximum velocities; thus, if a channel whose area is 21 square feet, has by observation a central surface velocity of 35 feet per minute, the mean velocity by the Table is 29.1 feet, and the discharge will be  $29.1 \times 21 = 705.6$  cubic feet, or  $705.6 \times 6.23 = 4396$  gallons per minute.

TABLE 14.—For OPEN CHANNELS, CANALS, and RIVERS, giving the MEAN VELOCITY throughout the SECTION, corresponding to observed CENTRAL SURFACE VELOCITIES.

Surface Velocity	Mean Velocity						
1	.81	26	21.81	51	42.81	76	63.81
2	1.03	27	22.63	52	43.63	77	64.63
3	2.52	28	23.52	53	44.52	78	65.52
4	3.90	29	24.90	54	45.90	79	66.90
5	4.2	30	25.2	55	46.20	80	67.2
6	5.01	31	26.06	56	47.01	81	68.04
7	5.83	32	26.83	57	47.83	82	69.83
8	6.72	33	27.72	58	48.72	83	70.72
9	7.50	34	28.50	59	49.50	84	70.50
10	8.4	35	29.4	60	50.4	85	71.40
11	9.21	36	30.21	61	51.21	86	72.21
12	10.09	37	31.09	62	52.12	87	73.09
13	10.92	38	31.92	63	52.92	88	73.92
14	11.76	39	32.76	64	53.76	89	74.76
15	12.60	40	33.6	65	54.6	90	75.6
16	13.44	41	34.44	66	55.44	91	76.44
17	14.28	42	35.28	67	56.28	92	77.28
18	15.12	43	36.12	68	57.12	93	78.12
19	15.96	44	36.96	69	57.96	94	78.96
20	16.8	45	37.8	70	58.8	95	79.80
21	17.64	46	38.64	71	59.64	96	80.64
22	18.48	47	39.48	72	60.48	97	81.48
23	19.32	48	40.32	73	61.32	98	82.32
24	20.16	49	41.16	74	62.16	99	83.16
25	21.0	50	42.0	75	63.00	100	84.00

(51) "Head due to Velocity in Open Channels"—When a stream leaves the still water of a lake or reservoir, as in Fig. 30,

at a given velocity, there will be a certain loss of head to generate that velocity, that is to say, the stream at F must be lower than the still water at E in order to create the velocity required at G. In a case like the Figure, the bottom of the channel at F being at the same level as the bottom of the reservoir at E, and with a well-rounded entrance, the velocity would be .96 of that due to gravity, and the same co-efficient would apply to the water-way of a sluice-gate, like Fig. 31, if the gate is drawn up completely out of the water and to the openings of a bridge with pointed piers, as at Fig. 32, the conditions being evidently similar in all the three cases. With similar conditions, but with square corners at the sides of the inlet opening, as in Fig. 34, the bottom of the channel being still at the same level as that of the reservoir, the velocity at G would be .86 of that due to gravity, or to the difference of level between E and G, and the same co-efficient applies to the openings of a bridge with square piers as in Fig. 33.

With an opening in a sluice-gate of small thickness, as at Fig. 35 the head of water being above the lower edge of the gate the velocity is only .635 of that due to gravity, a contraction (2) occurring on all the four sides of the aperture. If the gate be fully drawn up, the opening becomes a weir, as at Fig. 36, then contraction occurs on three sides only, and the co-efficient rises to .667. These co-efficients are given by Eytelwein, and Table 15 gives the velocities for different heads calculated by them.

(52) "*Head to overcome Friction of Channel*"—When the channel is a long one, there is not only a loss of head due to the velocity, but also a further loss by friction against the sides and bottom. Where the channel is of equal cross sectional area from end to end, the loss of head increases uniformly from end to end, and the surface of water has a certain slope or fall per yard or per mile. Fig. 37 shows the section of a water-course in which the fall from the still water in the reservoir at A to the point B is due to the velocity at B, and this would be the same whatever the length of the channel, its amount varies with the form of the entrance as explained in (51). From B to

C there will be a regular slope when the area of the channel is uniform, and the fall C D is due to friction for the length B C

TABLE 15.—Of the Velocities in FEET per Second, due to given HEADS

Head in Inches	A. Coeff. 1.6	B. Coeff. 1.8	C. Coeff. 2.0	D. Coeff. 2.25	Head in Inches	A. Coeff. 1.6	B. Coeff. 1.8	C. Coeff. 2.0	D. Coeff. 2.25
1	29	2781	2191	18115	1	2 317	2 2221	1 9930	1 4713
2	41	3936	3221	2603	11	2 540	2 4871	2 2270	1 6116
3	53	5368	4794	3643	12	2 767	2 7231	2 4333	1 8015
4	62	7472	70.2	5.07	22	3 065	2 9121	2 6569	1 9463
5	1 0	9600	8600	6350	2	3 276	3 145	2 8174	2 0403
6	1 153	1 1117	97.9	7733	21	3 475	3 336	2 9885	2 2000
7	1 293	1 2132	1 1110	8221	21	3 663	3 516	3 1502	2 3260
8	1 418	1 3613	1 2193	9001	21	3 812	3 658	3 2011	2 4397
9	1 532	1 4707	1 3173	9723	3	4 012	3 851	3 4503	2 5176
10	1 638	1 5723	1 4087	1 0101	3½	4 176	4 009	3 5914	2 6317
11	1 737	1 6673	1 4938	1 1030	3½	4 331	4 161	3 7272	2 7521
12	1 831	1 7577	1 5747	1 26.7	3½	4 480	4 306	3 8580	2 8186
13	1 921	1 8442	1 652	1 21.8	4	4 630	4 449	3 9444	2 9120
14	2 006	1 9253	1 725	1 27.9	4½	4 914	4 717	4 2260	3 1204
15	2 089	2 0015	1 796	1 32.0	5	5 180	4 973	4 455	3 2893
16	2 167	2 0803	1 863	1 376	5½	5 433	5 216	4 672	3 450
17	2 213	2 1533	1 920	1 421	6	5 675	5 418	4 881	3 6036

(53) This fall may be calculated by the following rule —

$$F = \frac{\left(\frac{C}{A}\right)^2 \times L \times P}{874520 \times A},$$

In which L = length of the channel in yards

A = cross sectional area of the stream in square feet

P = the perimeter, or wetted border in feet

F = the fall, or difference of level at the two ends of the channel in inches

C = cubic feet discharged per minute

Thus, in the case shown by Fig. 38, A being  $6 \times 2.5 = 15$  square feet,  $P = 2.5 + 6 + 2.5 = 11$  feet, say that with such a channel 1760 yards, or one mile long, we require the fall to

discharge 1105 cubic feet per minute then by the rule we

$$\text{have in our case } \frac{\left(\frac{1105}{15}\right)^2 \times 1760 \times 11}{874520 \times 15} = 8 \text{ inches fall}$$

(54) To this has to be added the head for the velocity at entry, or A B in Fig. 37. The mean velocity being  $\frac{1105}{15} =$

73 66 feet, the maximum (50) will be  $\frac{73 \frac{66}{84}}{.84} = 87 \frac{7}{8}$  feet per minute, or 1 46 foot per second, the head for which, with square corners, is given by Col O of Table 16 at about  $\frac{1}{2}$ -inch. Then for a channel one mile long, the total head will be  $8 + \frac{1}{2} = 8\frac{1}{2}$  inches, for  $\frac{1}{8}$ th of a mile, or 220 yards,  $1 + \frac{1}{2} = 1\frac{1}{2}$  inch, and for 110 yards,  $\frac{1}{2} + \frac{1}{2} = 1$  inch. In the last case the head for velocity is equal to the head for friction.

(55) When the fall is given, and the discharge has to be calculated the rule becomes —

$$Q = \left( \frac{874620 \times F \times A}{L \times P} \right)^{\frac{1}{2}} \times A$$

Thus, with the same channel as before, 1760 yards long, and a fall of 12 inches, the discharge would be  $\left( \frac{874620 \times 12 \times 15}{1760 \times 11} \right)^{\frac{1}{2}} \times 15 = 1353$  cubic feet per minute. We have omitted in this case to allow for the head due to velocity, and where the channel is a long one, the omission will not cause a serious error, with short channels, however, it must not be neglected.

(56) When, with a given total head, we have to calculate the discharge by a channel so short that the head for velocity has to be considered as well as that due to friction, the question does not admit of a direct solution, because we cannot tell beforehand in what proportions the head at disposal has to be divided between the two. The best course in that case is to assume a discharge, and calculate, as in (53) and (51) the head for friction and the head for velocity with that discharge. Then

applying the law (27) that the discharges are directly proportional to the square roots of the respective heads, we may obtain the true discharge with the given head. Thus say that with the channel (Fig. 38) 50 yards long, the total head at disposal was 2 inches, and that we have to calculate the discharge. Say we assume it at 1000 cubic feet; then the head for friction would be

$$\frac{\left(\frac{1000}{15}\right)^2 \times 50 \times 11}{874520 \times 15} = .186 \text{ inch}$$

The mean velocity being  $\frac{1000}{15} = 66\frac{2}{3}$ , the maximum will be  $\frac{66\frac{2}{3}}{1.41} = 72\frac{5}{9}$  feet per minute, or 1.22 foot per second. The head for which by Col. C in Table 13 is about  $\frac{1}{4}$  or .437 inch; the total head for 1000 cubic feet is therefore,  $.186 + .437 = .623$  inch; hence the discharge with 2 inches head will be  $1000 \times \sqrt{2} = 1000 \times 1.414 = \dots \dots \dots$

The use of this Table may be illustrated by the following examples — Say we calculate by it the discharge of the channel (Fig 38) with a fall of 12 inches per mile as in (55). The hydraulic radius in our case is  $\frac{15}{11} = 1\ 363$  foot, the nearest radius to which in the Table we find to be 1 3 and 1 4, and the corresponding velocities under the fall of 12 inches per mile are 88 1 and 91 4 respectively, interpolating between those numbers for our radius 1 363 we find the mean velocity to be about 90 2 feet, and the discharge  $90\ 2 \times 15 = 1353$  cubic feet per minute.

Again, to find the fall with the same channel 800 yards long for 1230 cubic feet per minute — The mean velocity being  $\frac{1230}{15} = 82$  feet per minute, we look between 1 3 and 1 4 radii in the Table for that velocity, and we find it to be under the fall of 10 inches per mile, or 00568 inch per yard, hence the fall in our case is about  $00568 \times 800 = 4\ 54$  inches for friction alone, or C D in Fig 87.

(58) Take another case, shown by Fig 40, of an open cutting with sloping banks, and say that we require the discharge with a fall of 8 inches per mile. The area being  $\frac{30+20}{2} \times 2\ 5 = 62\ 5$  square feet, and the border  $5\ 6 + 20 + 5\ 6 = 31\ 2$  feet the hydraulic radius is  $\frac{62\ 5}{31\ 2} = 2$ , which, by Table 30, with a fall of 8 inches per mile will have a velocity of 89 2 feet, and a discharge of  $89\ 2 \times 62\ 5 = 5575$  cubic feet per minute.

(59) "River Channels of irregular Cross section" — The application of the rules to the discharge of a stream of the natural irregular form of section may be illustrated by Fig 41. We found in (68) that the area was 27 74 square feet, taking say 2 feet in the compasses, and stepping along the border, we find it to measure about 21 5 feet the hydraulic radius is therefore,  $\frac{27\ 74}{21\ 5} = 1\ 3182$  foot. Then, with a fall of say 10 inches per

mile, Table 30 gives, opposite the radius of 1·1 (which is the nearest to the one we require), the mean velocity of 73·9 feet per minute, hence the discharge is  $73\cdot9 \times 27\cdot74 = 2050$  cubic feet per minute. With a very short channel, allowance should be made for velocity at entry, as explained in (56).

Table 30 may also be applied to the calculation of the discharge, &c., of common pipes running full, or to those of a square or other section, for an illustration of which see (36), also to culverts, &c., partially filled, see (62).

(60) "*Openings of Bridges, &c.*"—The head lost by a stream in passing through a bridge is principally that due to velocity alone, the length of the channel being in most cases so short as to have little influence on the discharge. The head for velocity may be calculated by Table 15, say we take the case (58) of the stream (Fig. 40) discharging 5575 cubic feet per minute, and passing through an opening at a bridge, say 8 feet wide and 3 feet deep. The area being  $8 \times 3 = 24$  square feet, the velocity will be  $\frac{5575}{24 \times 60} = 3\cdot87$  feet per second, which, with pointed piers (Fig. 32) will require by Col. B of Table 15, 8 inches head (A, B in Fig. 37). But, the stream approaches the bridge with a mean velocity of 89·2 feet, or a maximum (50) of  $\frac{89\cdot2}{84} = 106$  feet per minute, or 1·77 foot per second, the head due to which by the same Table is  $\frac{5}{6}$  inch. The head at the bridge is, therefore, reduced to  $3 - \frac{5}{6} = 2\frac{1}{6}$  inches, with square piers (Fig. 33), the head by Col. C is  $3\frac{1}{2}$  inches, or at the bridge  $3\frac{1}{2} - \frac{5}{6} = 3\frac{1}{6}$  inches.

(61) "*Submerged Openings*"—The velocity of discharge through a submerged opening A (Fig. 43) is governed by the difference of the level of water at the two sides of it or by H, and is not affected by the depth below the surface at which it is placed. Table 15 will give the velocity with small heads thus an aperture 2 feet  $\times$  1·5 foot = 3 square feet area, and with H = 5 inches, would, by Col. D of Table 15, discharge  $3 \times 2893 \times 3 = 9\cdot87$  cubic feet per second.

## PROPORTIONS, ETC., OF OVAL CULVERTS.

### Table 10.—Of the Proportions and Discrepancy Powers of Oval Clusters

This shows that in all cases where extreme accuracy is desired, the rule in (61) should be used, but that where the fall exceeds 8 or 10 inches per mile, Table 30 gives results sufficiently correct for most practical purposes.

(66) When the discharge is given, to determine the fall, the rule becomes

$$F = \frac{\left(\frac{C}{A} + 6.624\right)^3 - 42.8}{896100 \times A} \times L \times P$$

Thus the fall for friction with the same channel, Fig. 40, 2000 yards long to deliver 3000 cubic feet per minute would be

$$\frac{\left(\frac{3000}{62.5} + 6.534\right)^3 - 42.8}{896100 \times 62.5} \times 2000 \times 31.2 = 3.26, \text{ or } 3\frac{1}{2} \text{ inches.}$$

Adding the head due to velocity at entry (51), the mean velocity is  $\frac{3000}{62.5} = 48$ , and the maximum  $\frac{48}{84} = 57$  feet per minute, or  $.95$  foot per second, the head for which by Col. C of Table 15 is about  $\frac{1}{2}$  inch, the total head is therefore  $3\frac{1}{2} + \frac{1}{2} = 3\frac{3}{4}$  inches.

(67) Table 18 has been calculated by the following modification of Eytelwein's rule —

$$\frac{(V + 1089)^3 - 0118858}{8975} = R \cdot S$$

In which  $V$  = the mean velocity over the whole area in feet per second

$R$  = the hydraulic radius in feet, or  $\frac{\text{area in square feet}}{\text{border in feet}}$

$S$  = the slope, or  $\frac{\text{fall in inches}}{\text{length in inches}}$

By this Table approximately correct results may be obtained with less labour than by the rules.

1st To find the Velocity — Multiply the area of the channel in square feet by the fall in inches, and divide the product by the border in feet multiplied by the length of the channel in inches find the nearest number thereto in Col. B of Table 18, and oppo-

$$C = \left( \frac{896400 \times \Gamma \times A}{L \times P} + 42.8 \right)^{\frac{1}{2}} - 6.534 \times A,$$

In which L = length of the channel in yards

- „ A = cross sectional area of the stream in square feet
- „ P = the perimeter, or border of the channel in feet
- „ F = the fall, or difference of level at the two ends of the channel in inches
- „ C = cubic feet discharged per minute

(65) Thus, say that we require the discharge by the channel, Fig 40, 1 mile long, with a fall of 1 inch only, then L = 1760, A = 62.5, P = 31.2, as in (58), and  $\Gamma = 1$ , and the discharge will be  $\left( \frac{896400 \times 1 \times 62.5}{1760 \times 31.2} + 42.8 \right)^{\frac{1}{2}} - 6.534 \times 62.5 = 1629.8$  cubic feet per minute. We may compare this result with that given by the rule in (55), by which the discharge comes out  $\left( \frac{874520 \times 1 \times 62.5}{1760 \times 31.2} \right)^{\frac{1}{2}} \times 62.5 = 1972$  cubic feet per minute =  $\frac{1972}{1629} = 1.21$ , or 21 per cent difference. But with an increased head, the difference becomes less, and is reduced practically to nothing with large heads, as shown by Table 17

TABLE 17.—Of the DISCHARGE of an OPEN CHANNEL, Fig 40, calculated by DIFFERENT RULES

Fall in Inches per Mile	Calculated Discharge.		Difference per Cent.	By Table 30.		
	By Rule in (64)	By Rule in (55)		Velocity	Area	Discharge.
1	1629	1972	21.0	31.5 × 62.5 = 1969		
2	2444	2783	14.1	44.6 ..		2783
3	3073	3416	11.1	54.6 ..		3113
4	3556	3943	10.9	63.0 ..		3933
5	4074	4400	8.2	70.5 ..		4106
6	4499	4830	7.3	77.2 ..		4825
8	5253	5577	6.2	89.2 ..		5575
10	5918	6235	5.3	99.7 ..		6231
12	6510	6831	4.9	109.2 ..		6825
24	9380	9649	3.0	151.4 ..		9650
36	11576	11831	2.2	189.1 ..		11819

This shows that in all cases where extreme accuracy is desired, the rule in (64) should be used, but that where the fall exceeds 8 or 10 inches per mile, Table 30 gives results sufficiently correct for most practical purposes.

(66) When the discharge is given, to determine the fall, the rule becomes

$$F = \frac{\left(\frac{Q}{A} + 6.534\right)^2 - 42.8}{896400 \times A}$$

Thus the fall for friction with the same channel Fig. 40, 2000 yards long to deliver 3000 cubic feet per minute would be

$$\frac{\left(\frac{3000}{62.5} + 6.534\right)^2 - 42.8 \times 2000 \times 31.2}{896400 \times 62.5} = 3.26, \text{ or } 3\frac{1}{2} \text{ inches.}$$

Adding the head due to velocity at entry (51), the mean velocity is  $\frac{3000}{62.5} = 48$ , and the maximum  $\frac{48}{84} = 57$  feet per minute, or

.95 foot per second, the head for which by Col C of Table 15 is about  $\frac{1}{2}$  inch, the total head is therefore  $3\frac{1}{2} + \frac{1}{2} = 3\frac{3}{4}$  inches.

(67) Table 18 has been calculated by the following modification of Eytelwein's rule —

$$\frac{(V + 1089)^2 - 0118858}{8975} = R.S$$

In which V = the mean velocity over the whole area in feet per second

R = the hydraulic radius in feet or  $\frac{\text{area in square feet}}{\text{border in feet}}$

S = the slope or  $\frac{\text{fall in inches}}{\text{length in inches}}$

By this Table approximately correct results may be obtained with less labour than by the rules.

1st. To find the Velocity — Multiply the area of the channel in square feet by the fall in inches, and divide the product by the border in feet multiplied by the length of the channel in inches and find the nearest number thereto in Col B of Table 18, and oppo-

site to that number in Col A is the required velocity. Thus for the case in (65) we have  $\frac{62.5 \times 1}{31.2 \times (1760 \times 36)} = .0000316$ , the nearest number to which is .00003043 opposite .425 foot per second. By interpolation we may obtain a nearer approximation, for, as R/S varies nearly as  $V^2$ , we have  $(\frac{425^2 \times .0000316}{00003043})^{\frac{1}{2}}$  or  $(\frac{180625 \times .316}{.3043})^{\frac{1}{2}} = .4331$  foot per second, hence the discharge comes out  $.4331 \times 60 \times 62.5 = 1624$  cubic feet per minute, or practically the same as by the rule (65).

TABLE 18 —For the DISCHARGE of CANALS, RIVERS, &c., by EYTELWEIN'S RULE

Mean Velocity in Feet per Second.	R.S.	Mean Velocity in Feet per Second.	R.S.
A	B	A	B
025	0000006734	6	00005460
05	000001489	65	00006284
075	000002144	7	00007158
1	000003533	75	00008087
125	000004771	8	00009072
15	000006144	85	00010112
175	000007656	9	0001121
2	000009307	.05	0001236
225	0000111	1 0	0001357
25	00001303	1 1	00016146
275	00001510	1 2	0001895
3	00001730	1 3	00021984
3 <sup>2</sup> 5	00001966	1 4	0002524
35	00002214	1 5	00028703
375	00002477	1 6	00032402
4	00002753	1 7	0003632
425	00003043	1 8	0004047
45	00003318	1 9	000448
475	00003666	2 0	0004913
5	00003928	2 5	000707
55	00004705	3 0	001075

2nd To find the F<sup>1</sup>  
given area, and by 60,

given discharge  
the mean velocity

per second; fall the nearest number to that in Col. A, which, multiplied by the longer in feet and by the length of the channel in inches, and divided by the area in square feet will give the fall in inches. Thus, for the case in (66) we have  $\frac{2000}{62.5} = 48$  feet per minute, or  $\frac{48}{60} = 8$  feet per second, the tabular number for which is .0000072, then

$$\frac{.0000072 \times 31.2 \times (2000 \times 36)}{62.5} = 3.26 \text{ inches fall},$$

as before.

68. "Case of a Mill-stream"—As an example of the practical application of the rules, we will take a case in which it is desired to utilize a stream of water for driving a corn-mill. Say we have a stream 1500 yards long with a total fall of 6 ft. 6 in. from the tail of the preceding mill. We have first to ascertain the quantity of water at disposal selecting a spot where the current appears to be tolerably uniform for some 100 feet, and a season when the quantity is an average one according to local authorities, say we take it at a point 21 feet wide as in Fig. 11. We have then to obtain the area of the stream, and to do that, may divide the width into eight equal spaces of 3 feet each, as in the Figure, which may be done conveniently by stretching a tape across the stream then we measure the depths midway between those divisions or at 1.5 foot, 4.5, 7.5 feet, &c., &c., using a measuring rod with a flat board about 7 or 8 inches square at the end of it, to prevent penetrating the soft bottom, and thus we obtain the series of measurements given in the figure, the mean of which we find to be 1.156 foot the area is therefore  $1.156 \times 21 = 27.71$  square feet. To find the velocity, two lines may be stretched across the stream near the surface, and say a "chain" or 66 feet apart, and a float being placed a few yards above the highest one, and in the centre of the width, or rather where the velocity is observed to be greatest, the exact time in passing from line to line is carefully noted. This float should be a small piece of thin wood, say only  $\frac{1}{2}$ -inch thick, so

as to be almost wholly immersed, and thus expose little surface to the action of the wind. Say that the float travels the 66 feet in 20 seconds, in one minute therefore it would be  $\frac{66 \times 60}{20} =$  198 feet. This being the maximum velocity, the mean (50) over the whole area would be  $198 \times .84 = 166$  feet per minute, hence the discharge is  $166 \times 27.74 = 4600$  cubic feet per minute.

(69) The total fall is 6 feet 6 inches, allowing 6 inches for the fall of the stream itself, the net fall at the wheel will be 6 feet, a cubic foot of water weighing 62.3 lbs., the horse-power being 33,000 foot pounds, and allowing that a breast-wheel yields 50 per cent, or  $\frac{5}{6}$  of the gross power of the water, we have  $\frac{4600 \times 62.3 \times 6 \times \frac{5}{6}}{33000} = 26$  horse power. A pair of

4-foot stones, grinding 4 bushels of corn per hour, requires about 4 horse-power, and a dressing machine about 6 horse, if we allow four pairs of stones, we should require  $16 + 6 = 22$  horse-power, leaving 4 horse-power for the mill gearing and small machines, &c. The diameter of the water-wheel may be about 2.5 times the fall, say 15 feet, and the speed of its circumference being 4 feet per second, or 240 feet per minute, and the depth of the bucket 1.5 foot, the width of the wheel would be  $\frac{4600}{240 \times 1.5} = 12.8$ , say 13 feet. With other kinds of water-wheel the duty would be different a good overshot wheel would give from 70 to 80 per cent, a breast-wheel from 45 to 60, and an undershot, in which the water acts only by its impulse, from 27 to 30 per cent.

(70) The channel must now be altered, so as to deliver 4600 cubic feet per minute, with a fall of 6 inches in 1500 yards or  $\frac{1760 \times 6}{1500} = 7$  inches per mile. When altered to the form

A, B, C, D, the area will be  $\frac{21 + 12}{2} \times 3 = 64$  square feet, the mean velocity to discharge 4600 cubic feet will be  $\frac{4600}{64} = 72$ .

feet per minute, the border is  $6\frac{7}{8} + 12 + 6\frac{7}{8} = 25\frac{1}{4}$  feet, and the hydraulic radius  $\frac{51}{25\frac{1}{4}} = 2.126$  feet. Then by Table 80 between 2 and 2.2 radii, the velocity 85.2 feet is found to be under the fall of 7 inches per mile, the fall we allowed. It should be observed that it is imperative that the slope shall be uniform from end to end, at least where the area of the channel is uniform.

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## CHAPTER IV

### ON WEIRS, OVERFLOW-PIPES, &c

(71) "Weirs"—Fig. 36 shows a weir arranged for the purpose of gauging experimentally the quantity of water passing down the stream. A is a plate of thin iron with a notch cut out of it wide enough by estimation to carry off the water with a moderate depth of overfall, this is screwed to a thick plank B, to obtain the requisite stiffness for the plate, and the whole is fixed in the stream as shown. C is a stake with a flat and level top, which is driven into the bed of the stream to such a depth that its top is exactly level with the lip of the weir, and the depth of water flowing over is measured by a common rule held on its summit. The proper distance of the stake from the weir depends on the quantity of water to be dealt with, in small weirs it may be from 1 to 2 feet, in very large ones 20 to 25 feet. The object is to place it far enough away to avoid the curvature of surface which the water suffers as it approaches the weir, as shown by the Figure. There is some uncertainty in measuring by a rule in the manner indicated, arising from the capillary attraction causing the water to adhere to the rule and to rise above its true height. A more correct method is to use Francis's hook gauge, a rough modification of which is shown by Fig. 36. The stake J is, in this case, driven to such a depth that its top is at a height convenient to the eye, say 30 inches above the level of the lip of the weir, then a rough hook gauge D, formed of

wood about 1 inch thick, is cut in the form shown, the end E being flat and level, and the length EF made exactly equal to GH or 30 inches. The hook-gauge is held against the stake, and carefully adjusted, by the hook at E being first immersed, and then raised until it just coincides with the surface of the water, the depth of overflow is then given by the distance from the top of the stake to the top of the gauge at F, measured by a rule, &c.

(72) With a thin plate, and depths thus measured from still water, we have the following rules —

$$G = d \times \sqrt{d} \times l \times 2.67$$

$$l = \frac{G}{d \times \sqrt{d} \times 2.67}$$

$$d = \left( \sqrt{\frac{G}{l \times 2.67}} \right)^2$$

In which G = gallons discharged per minute

" d = depth of overflow in inches.

" l = length of weir in inches

Thus, with 2 inches overflow, a weir 72 inches long discharges  $2 \times 1.4142 \times 72 \times 2.67 = 613.7$  gallons per minute, again,

to discharge 691 gallons per minute, with 3 inches overflow, we should require a length of  $\frac{691}{3 \times 1.732 \times 2.67} = 50$  inches, and

again, to find the depth of overflow to carry 1282 gallons, with

a length of 60 inches we have  $\frac{1282}{60 \times 2.67} = 8$ , then  $\sqrt[3]{8} = 2$ ,

and  $2^2 = 4$  inches, the depth required. Table 19 has been calculated by these rules, and its use may be illustrated by the examples just given, thus with 2 inches overflow the Table gives 7.552 gallons per inch, and a weir 72 inches wide will discharge  $7.552 \times 72 = 543.7$  gallons, a weir with 9 inches overflow

discharges 19.87 gallons per inch of width, and for 691 gallons we require a length of  $\frac{691}{19.87} = 35$  inches, a weir 35 inches

long discharging 1282 gallons is equal to  $\frac{1282}{60} = 21 \cdot 36$  gallons per inch wide, which by the Table is due to 4 inches overflow, &c.

TABLE 19.—Of the DISCHARGE of WATER over WEIRS, 1 inch wide,  
 in GALLONS per MINUTE

(73) "Effect of Thickness of Crest"—When the lip of the weir has a considerable thickness, which is frequently a practical necessity, the discharge will be less than with a thin plate, a loss arising from friction. Mr Blackwell's experiments, made on a large scale, and with depths of overfall ranging from 1 inch to 14 inches, give us the following coefficients, by which Table 19 may be adapted to the forms commonly met with in practice —

	Ratio of Discharge
Thin plate, weir 10 feet long	1.000
P	815
C	712
-	700

Thus, say we have a river-weir 30 feet wide, with  $6\frac{1}{2}$  inches overfall, the crest having a slope of 1 in 12, then the discharge will be  $44.25 \times 360 \times 76 = 12,107$  gallons per minute, or  $\frac{12107}{628} = 1943$  cubic feet

(74) Table 19 may be applied to rectangular apertures like Fig 35, for the discharge in such a case is the difference between two weirs, A, B, C, D, and A, E, F, D, say the head to the top of the aperture (A, B) is  $16\frac{1}{2}$  inches, and to the bottom (A, E) 22 inches, and that the width (E, F) is 20 inches. Then, by Table 19, 22 inches = 275.5 gallons per inch, and  $16\frac{1}{2}$  inches = 179.0 gallons, the difference is, therefore,  $275.5 - 179.0 = 96.5$ , and the discharge  $96.5 \times 20 = 1930$  gallons, but as contraction occurs on four sides in this case, see (51), the real discharge would be  $1930 \times .635 = 667 = 1837$  gallons per minute. The coefficients in (73) do not apply to apertures with large heads.

Similarly we may determine the discharge of round apertures, or approximately of any regular figures, which will not differ materially from that of a circumscribing rectangular opening, reduction being made for the true area of the figure whose discharge is required. Thus, say we require the discharge of a

circular aperture 12 inches diameter, the head measured from the upper edge of the orifice being 14 inches, therefore, 26 inches above the lower edge. Here we have  $351 \frac{1}{2} - 139 \frac{8}{9} = 214 \frac{2}{9}$  gallons per inch wide, and if the aperture were rectangular it would discharge  $214 \cdot 2 \times 12 = 2570 \frac{4}{9}$  gallons, but being circular its area is  $\pi \cdot 7851$ , that of a circumscribing rectangle being 100, and the true discharge is  $2570 \frac{4}{9} \times 7851 \times 635 = 667 = 1922$  gallons per minute.

(75) "Effect of Velocity of Approach to Weirs, &c"—We have so far supposed that the head has been measured from still water, or that the channel was of very large area in proportion to the discharging orifices. When the channel is of small area, the water will have a sensible velocity as it approaches the aperture, which will increase the discharge, and correction must be made for it by adding to the measured head, that due to the observed velocity of approach. Table 15 gives the head due to a range of velocities such as are likely to be met with in ordinary practice, thus, in the case of a weir 60 inches wide, with  $8\frac{1}{2}$  inches overfall, the discharge =  $18 \cdot 42 \times 60 = 1105 \frac{2}{9}$  gallons, but if the velocity of approach had been 66 feet per minute or 11 foot per second, we find the head due to that velocity in Col. B =  $\frac{1}{2}$  inch, and the head on the weir becomes  $3\frac{1}{2} + \frac{1}{2} = 3\frac{3}{4}$ , and the discharge  $20 \cdot 37 \times 60 = 1222$  gallons. More strictly, it is the difference between two weirs with the respective overfalls of  $\frac{1}{2}$  inch and  $3\frac{1}{4}$ , or  $(20 \cdot 37 - 3338) \times 60 = 1202$  gallons, instead of  $1105 \frac{2}{9}$  gallons, as we found it for still water.

(76) "Correction for Short Weirs"—The rules in (72) assume that the discharge of a weir is simply proportional to its length. This is not strictly correct, in ordinary cases where the weir is narrower than the channel the issuing stream suffers contraction at the two ends, by which its length is virtually reduced, and as this contraction is about the same with all lengths its effect is proportionally greater with short weirs than with long ones. The experiments of Francis show that the effect of contraction at both ends is to reduce the effective length 0.2 inch for each inch in depth of overfall, or 1 inch with 5 inches deep, 2 inches with 10 inches deep, &c. With 5 inches overfall, and weirs

## OVERFLOW-PIPES TO TANKS.

TABLE 20.—The Discharge of Overflow Pipes for Tanks, &amp;c.

Diameter of Pipe in Inches	Diameter of the Trumpet Mouth in Inches										18
	2	3	4	5	6	7	8	9	10	11	
4	6	9	12	15	18	21	24	27	30	33	47
3	11	10	22	27	32	38	43	48	54	63	53
2	17	25	31	42	50	59	67	75	84	92	86
1	27	33	47	57	70	82	91	106	117	129	134
14	31	46	62	77	92	108	123	139	154	170	140
13	39	59	78	97	116	136	155	175	194	214	164
12	47	71	95	119	142	166	190	214	237	261	183
11	55	85	113	142	170	198	227	255	283	312	216
10	63	100	133	166	199	232	265	299	332	363	217
9	71	110	155	194	233	271	310	349	388	427	217
8	79	116	161	204	246	282	319	352	392	431	217
7	87	124	171	218	262	305	349	391	436	480	217
6	95	131	174	218	265	314	361	413	460	523	217
5	103	140	181	220	275	320	375	430	482	550	217
4	111	148	187	214	265	316	371	425	479	545	217
3	119	156	195	234	285	336	388	441	494	561	217
2	127	164	203	250	303	356	411	468	525	592	217
1	135	172	211	258	311	364	421	478	535	602	217
14	143	180	218	265	318	371	428	485	542	609	217
13	151	188	226	273	326	379	436	493	550	617	217
12	159	196	234	281	334	387	444	501	558	625	217
11	167	204	242	289	342	395	452	509	566	633	217
10	175	212	250	297	350	403	460	517	574	641	217
9	183	220	258	305	358	411	468	525	582	649	217
8	191	228	266	313	366	419	476	533	590	657	217
7	199	236	274	321	374	427	484	541	598	665	217
6	207	244	282	329	382	435	492	549	606	673	217
5	215	252	290	337	390	443	499	556	613	680	217
4	223	260	298	345	398	451	508	565	622	687	217
3	231	268	306	353	406	459	516	573	630	694	217
2	239	276	314	361	414	467	524	581	638	705	217
1	247	284	322	369	422	475	532	589	646	712	217

5, 10, 20, 50, and 100 inches long, Table 19 gives 149, 298, 597, 1492, and 2985 gallons per minute, but deducting one inch from all those lengths, they are reduced to 4, 9, 19, 49, and 99 inches, and the discharges become 119, 268, 567, 1462, and 2955 gallons. Francis gives a rule for weirs with thin plates, of which the following is a modification —

$$G = 24953 \times (l - 0.1nd) \times d^3$$

In which  $n$  = the number of end contractions (usually two), and the rest as in (72). Where the weir is the full width of the channel,  $n = 0$ . By this rule, with the real lengths given above, the discharges come out 112, 251, 530, 1367, and 2762 gallons, which are rather less than with the reduced lengths by Table 19.

(77) "Overflow-pipes to Tanks, &c"—The rules and Table for weirs apply also with approximate correctness to an overflow-pipe to a tank, as in Fig. 46, which may be considered as a circular weir whose length is equal to the circumference of the trumpet-mouth. The following rules will give the same result more directly —

$$G = D \times \sqrt{D} \times d \times 8.4$$

$$d = \frac{G}{8.4 \times D \times \sqrt{D}}$$

$$D = \left( \sqrt[3]{\frac{G}{8.4 \times d}} \right)^2,$$

In which  $d$  = the diameter of the trumpet mouth in inches,  $D$  = depth of water over the lip (measured from still-water) in inches, and  $G$  = gallons discharged per minute. Table 20 has been calculated by this rule. The size of the discharge pipe A must be determined by the ordinary rules, with short pipes the discharge is governed principally by the head due to velocity, which is given by Table 1 rather than Table 2 for a pipe of this form. For tanks 3 feet deep, and with a discharge-pipe of that length, Table 21 gives the maximum discharge. Say we had to provide for 400 gallons per minute —Table 21 shows that

4 inches is the smallest size of pipe admissible, and allowing  $2\frac{1}{2}$  inches for overflow, Table 20 gives 12 inches for the least diameter of trumpet-mouth. We must allow some margin for contingencies, and in such a case, the lip of the trumpet-mouth should not be less than 3 inches below the top of the tank, and thus 3 inches is practically lost in the useful depth of the tank.

TABLE 21.—OF THE MAXIMUM DISCHARGE OF VERTICAL PIPES 3 FEET LONG.

Diameter of Pipe in Inches.	Maximum Discharge in Gallons per Minute.	Diameter of Pipe in Inches.	Maximum Discharge in Gallons per Minute.
1	19	3½	303
1½	45	4	400
2	88	5	630
2½	145	6	920
3	220	7	1300

(78.) Fig. 47 shows a simple contrivance of the late Mr. Appold, by which this loss may be avoided, and the water-level not allowed to rise more than about  $\frac{1}{8}$ th of an inch above the lip of the trumpet-mouth, even when the descending pipe is discharging full-bore. B is a dished cover of sheet copper, &c., supported on four brackets C, C, cast on the pipe, so that its lip at D is at the same level as the lip of the trumpet-mouth. When the water rises to that level, it does not immediately flow over when the lip is dry, but rises perhaps  $\frac{1}{8}$ th of an inch above it, and then, suddenly overflowing, creates a partial vacuum under the cover, causing the water to rise there above the level of the water in the tank and filling the pipe full-bore. The air under cover is swallowed up by the rush of the water, and the maximum quantity which the pipe can carry is delivered. This continues till the water being drawn down below the lip of the cover a small amount ceases, to be again repeated. The action depends on the suction effect if the bore is not much larger than the pipe.

necessary. It is usual to construct the pipe so as to serve as a wash-out valve, the joint at the bottom being turned and bored to fit water-tight.

(79) "*Overflows to Fountains*"—In ornamental fountains with shallow basins it is important that the water-level should fluctuate as little as possible, hence the form of overflow-pipe just described is specially applicable to such cases. It is generally desirable that the pipe should be concealed, which may be done by fixing it in a small supplementary cistern by the side of the fountain basin, with a large passage between them. For small fountains with say 100 gallons per minute, an inverted overflow-pipe may be used, as in Fig 42, a short pipe A, which serves also as a waste-pipe to empty the basin when necessary by the cock B, carries the overflow trumpet-mouth C. Say we have 100 gallons, then with a 6 inch pipe at A, the head for velocity at entry would be about 1 inch, and with a 12 inch trumpet mouth the head for overflow, by Table 20, is also 1 inch, so that the water-line would fluctuate 2 inches. The cock B may be of smaller size, say 3 inches, the end of the pipe being reduced to suit it. With care, such an arrangement might be used for a very large quantity, by adjusting the cock so as to carry rather less than the supply, leaving the trumpet mouth to carry off the surplus and regulate the level.

(80) "*Common Overflow-pipe*"—When an overflow takes the form of a short pipe inserted in the side of a cistern as in Fig 45, and the water to be carried off is just sufficient to fill the pipe, the discharge will be given approximately by the following rule—

$$G = d^{1.5} \times 3.2,$$

In which  $G$  = gallons discharged per minute

„  $d$  = diameter in inches

Table 22, which has been calculated by this rule, may also be useful for another purpose. It sometimes happens that the only datum which an engineer obtains as a basis for rough estimates is, that a spring or stream delivers "about as much as a pipe of a certain size would carry." This, of course, is very indefinite, but in most cases it means the amount which a pipe would dis-

charge without extra pressure, as in Fig. 15 and Table 22: thus an 8-inch pipe just filled delivers about 580 gallons per minute: —the pipe in (37) was observed to be nearly filled with the issuing stream when discharging 564 gallons.

TABLE 22.—OF THE DISCHARGE OF OUTLET-PIPES, FIG. 45

Diameter Inches.	Gallons per Minute.	Diameter, Inches.	Gallons per Minute.	Diameter Inches.	Gallons per Minute.
1	3.2	5	179	13	1950
1½	8.8	6	283	14	2446
2	18.1	7	413	15	2788
2½	31.6	8	540	16	3277
3	50.0	9	778	17	3814
3½	73.3	10	1012	18	4400
4	112.1	11	1244	19	5037
4½	138.0	12	1600	20	5725

## CHAPTER V.

### ON THE STRENGTH OF WATER-PIPES—RAINFALL, &c., &c.

(81) "Strength of Thick Pipes"—The strength of pipes to resist an internal pressure is not simply proportional to the thickness of metal. The material stretches or extends under a tensile strain, and the result of extension is, that the inside metal is more strained than that of the outside, and that thick pipes are weaker in proportion to their thickness than thin ones. Barlow has given the following rules:—

$$T = \frac{R \times P}{b - P}$$

$$P = \frac{S \times T}{R + T}$$

$$S = \frac{(R + T) \times P}{T};$$

In which  $S$  = the cohesive strength of the metal per square inch

"  $P$  = the internal pressure per square inch, in the same terms as  $S$

"  $R$  = the radius of the inside of the pipe in inches

"  $T$  = the thickness of metal in inches

For cast-iron  $S$  may be taken at 7 142 tons, or 16,000 lbs. per square inch, and with that strength we obtain the bursting pressure given by Table 23, which shows that with a 10 inch pipe a thickness of 10 inches gives only four times the strength due to a thickness of 1 inch.

TABLE 23.—Of the STRENGTH of a 10-INCH CAST IRON PIPE to RESIST INTERNAL PRESSURE, in Tons per Square Inch

Thickness in inches	1	2	3	4	5
Pressure by Barlow's rule	1 19	2 01	2 63	3 17	3 5-
Pressure by exact calculation	1 226	2 161	2 896	3 483	3 972

Thickness in inches	6	7	8	9	10
Pressure by Barlow's rule	3 90	4 17	4 40	4 59	4 76
Pressure by exact calculation	4 337	4 722	5 019	5 273	5 5

Barlow's rule supposes that the extensions are simply proportional to the strain, which is not quite correct, by taking the true extensions we obtain the second series of bursting pressures given in the Table by a calculation which need not be here elaborated.

(62) *Strength of Thin Pipes* — Barlow's rule is quite inapplicable to comparatively thin pipes, such as are commonly used for water and gas, there are other and practical ones I suppose which that rule does not contemplate. With thin pipes at moderate pressures, we have to consider not only the thickness necessary to bear the pressure, but also that required to bear the traffic along the roads in which they are laid without fail. Again, although great care is taken to keep the centre central it is well known perfectly so; a pipe intended to be 1 inch thick is frequently

Table 24.—Of the Thickness and Weight of Cast-Iron Socket-Pipe to Bear Saturated Differnt Pressures of Water

Diameter in Inches	Length ex- clusive of Sockets	For Gas &c.			100 feet			250 feet			500 feet			750 feet			1000 feet		
		in. ft.	inch cwt qrs lbs																
1½	6 0	27	0 1 3	28	0 1 4	29	0 1 5	30	0 1 7	31	0 1 8	33	0 1 10	35	0 1 26	37	0 2 2	39	0 2 20
2	6 0	30	0 1 17	30	0 1 19	31	0 1 20	33	0 1 23	35	0 1 26	37	0 1 26	37	0 2 14	40	0 2 20	41	1 1 0
2½	6 0	32	0 2 1	31	0 2 3	33	0 2 7	35	0 2 11	37	0 2 14	41	1 0 19	44	1 1 18	51	1 3 18	51	1 3 18
3	9 0	32	0 3 18	33	0 3 21	35	1 0 8	38	1 0 9	41	1 0 19	44	1 1 0	51	1 3 18	53	3 1 24	53	3 1 24
3½	9 0	35	1 1 7	37	1 1 15	39	1 1 24	43	1 2 13	47	1 3 1	51	1 3 18	55	3 1 24	55	3 1 24	55	3 1 24
4	9 0	35	1 1 7	37	1 1 15	39	1 1 24	43	1 2 13	47	1 3 1	51	1 3 18	55	3 1 24	55	3 1 24	55	3 1 24
5	9 0	37	1 2 23	39	1 3 5	42	1 3 21	47	2 0 19	52	2 1 16	57	2 1 16	63	3 1 24	63	3 1 24	63	3 1 24
6	9 0	41	2 2 18	42	2 3 8	45	2 1 6	48	3 0 9	51	2 1 25	51	2 3 6	57	3 0 15	63	4 1 21	63	4 1 21
7	9 0	43	3 0 14	44	3 1 14	46	3 1 10	51	3 2 23	53	4 1 7	63	5 0 14	67	4 3 13	73	5 1 22	73	5 1 22
8	9 0	45	3 2 18	48	3 3 17	53	4 1 7	57	3 2 4	59	4 1 4	63	5 0 14	72	5 3 12	81	0 3 10	81	0 3 10
9	9 0	45	3 2 18	48	3 3 17	53	4 1 7	57	3 2 4	59	4 1 4	63	5 0 14	72	5 3 12	81	0 3 10	81	0 3 10
10	9 0	47	4 0 26	51	4 2 10	57	5 0 15	67	6 0 4	77	6 3 21	87	7 3 9	97	10 2 0	97	10 2 0	97	10 2 0
11	9 0	50	5 1 21	51	5 3 6	61	6 2 6	73	7 3 11	85	9 0 15	97	10 2 0	113	15 2 0	113	15 2 0	113	15 2 0
12	9 0	53	7 1 0	53	8 0 6	63	9 1 4	83	11 1 9	99	13 0 14	111	18 0	123	1 0	123	1 0	123	1 0
13	9 0	57	9 1 0	64	10 1 16	73	12 1 0	93	15 0 11	111	18 1	123	1 0	123	1 0	123	1 0	123	1 0
14	9 0	60	11 0 11	69	12 3 12	81	15 0 18	103	19 1 7	111	18 1	123	1 0	123	1 0	123	1 0	123	1 0
15	9 0	64	13 2 0	73	15 2 0	88	18 3 2	123	2 4	136	2 9	160	3 3	181	2 14	181	2 14	181	2 14
16	9 0	64	13 2 0	73	15 2 0	88	18 3 2	123	2 4	136	2 9	160	3 3	181	2 14	181	2 14	181	2 14
17	9 0	67	14 2 1	81	21 1	91	21 1	103	20 1 2	123	31 3 1	159	42 1 0	174	50 2 5	174	50 2 5	174	50 2 5
18	9 0	67	14 2 1	81	21 1	91	21 1	103	20 1 2	123	31 3 1	159	42 1 0	174	50 2 5	174	50 2 5	174	50 2 5
19	9 0	70	14 2 1	81	21 1	91	21 1	103	20 1 2	123	31 3 1	159	42 1 0	174	50 2 5	174	50 2 5	174	50 2 5
20	9 0	73	21 2 6	89	28 0 6	91	28 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
21	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
22	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
23	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
24	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
25	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
26	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
27	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
28	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
29	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
30	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
31	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
32	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
33	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
34	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
35	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
36	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
37	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
38	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
39	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
40	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
41	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
42	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
43	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
44	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
45	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
46	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
47	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
48	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
49	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
50	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
51	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
52	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
53	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
54	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
55	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
56	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
57	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0
58	9 0	75	23 2 16	93	32 0 6	95	32 0 6	103	35 0 0	123	35 0 0	159	49 1 0	174	57 1 0	174	57 1 0	174	57 1 0

$\frac{1}{8}$ ths at one side and  $\frac{5}{8}$ ths at the other, and of course the least thickness governs the strength of the pipe. And again, there are in most cases shocks arising from the closing of cocks, &c., against which it is necessary to provide adequate strength. In thin pipes, therefore, the determination of the thickness becomes a practical question, and we must obtain an empirical rule from experience. The rule may take the following form —

$$t = \left( \frac{\sqrt{D}}{10} + 15 \right) + \left( \frac{H \times D}{25000} \right),$$

In which  $D$  = the diameter of the pipe in inches.

"  $H$  = the safe head of water, in feet

"  $t$  = the thickness of metal in inches

Table 24 has been calculated by this rule, and we have also given the approximate weights from gas pipes in which the pressure is practically nothing, up to 1000 feet of water. Engineers usually specify the weight of their pipes rather than the thickness, leaving the founder to fix that for himself which long practice enables him to do with considerable precision. Of course absolute correctness cannot be attained, and should not be expected, a margin should be allowed, say one pound to the inch, either way, so that, for instance, a 10-inch pipe for 100 feet head, specified to weigh 4 cwt 2 qrs 10 lbs, as per Table 21, should not be rejected if its real weight is between 4 cwt 2 qrs 0 lbs and 4 cwt 2 qrs 20 lbs, &c. Founders consider this to be a fair allowance for variation in weight.

(83) "*Proportions of Socket pipes*" — The joints of water-pipes are usually made by sockets and spigots run with melted lead, and this is the best mode. Such pipes are easy to cast, and consequently cheap, the joints are more easily made than with flanges, and they admit a considerable departure from the strictly straight line which is sometimes very convenient. But to allow for this the sockets must be made of larger diameter than is necessary where the line is straight, and for this reason, perhaps, sockets are frequently made larger than they should be for making a good joint. For ordinary cases  $\frac{1}{8}$  inch in thickness or  $\frac{1}{4}$  inch in diameter will suffice for pipes of 3 inches diameter.

TABLE 27.—Of the PROPORTIONS of CAST IRON FLANGE PIPES

Diameter of Pipe	Diameter of Flange.	Thickness of Flange	No. of Bolts	Diameter of Bolts	Diameter of Circle of Bolts
inches	inches.	inches.		inches	inches
1½	4½	2	3	½	3½
2	5½	2	3	⅓	3½
2½	6	2	4	⅓	4½
3	6½	2	4	⅔	5
4	8	2	4	⅔	6½
5	9½	2	4	⅔	7½
6	10½	2	6	⅔	8½
7	12	2	6	⅔	10
8	13½	2	6	⅔	11½
9	14½	2	6	⅔	12½
10	16	1	6	⅔	13½
12	18½	1	6	⅔	16

(85) "*Strength of Lead Pipes*"—The strength of lead pipe may be calculated by Barlow's rule (81), taking the cohesive strength of drawn lead at 2745 lbs per square inch, as determined by direct experiment. Lead pipes are made of various weights to suit the varying requirements of practice, taking medium weights, and deducing the thickness therefrom, we obtain the following Table, in which the safe working pressure is taken at  $\frac{1}{5}$ th of the bursting strain —

Diameter of pipe	½	¾	¾	1	1½	1½	1½	2
Weight of pipe lbs per foot	1 33	1 47	1 67	2 80	4 33	6 0	6 75	6 0
Safe pressure feet of water	232	183	174	151	152	140	122	116

(86) "*Power of Horses, &c., in raising Water*"—The power of men, horses, &c., in raising water varies with the duration of the labour. The following Table gives the number of gallons raised 1 foot high per minute, with common deep-well pumps, and the mean velocity in feet per minute

Velocity	Hours per Day	4	5	6	8	10
176	Horse walking in a circle	1653	1480	1350	1169	1040
180	Pony or mule, ditto	1102	986	898	740	697
120	Bullock, ditto	1470	1314	1200	1010	930
157	Ass, ditto	457	410	374	323	290
220	Man, with winch pump	249	222	203	176	157
147	Ditto Contractor's pump	205	183	167	145	130

A good high pressure steam-engine should raise 3300 gallons 1 foot high per minute per nominal horse-power, the friction of the pumps being compensated by the excess of the indicated power over the nominal.

(87) "*Rainfall*"—The depth of rain in this country varies very much with the locality, the east coast is the driest, the annual rainfall being in Northumberland about 28.67 inches, diminishing thence gradually to 23 in Norfolk and to 19.8 in Essex, which is the minimum. Thence southward and westward it gradually increases to 25.6 in Kent, 30.64 in Sussex, 38.75 in Dorset, 48.3 in Devon, and 50.6 in Cornwall. The midland districts have a medium fall—Middlesex 24.1, Leicester 26.0, Hereford 29.27, Cheshire 31.3, &c., &c.

"*Heavy Rains*"—For town drainage and other purposes, we require to know the maximum fall of rain during storms. We find that in

1	5	15	30	45	60	120	180	minutes
the maximum fall of rain may be								
0.2	0.75	1.0	1.8	2.5	3.25	3.6	4	inches,
which is at the rate per hour of								
12	9	4	3.6	3.3	3.25	1.8	1.33	inches

"*Rain-water Tanks*"—Where it is desired to utilize as much as possible of the rain falling on a building the minimum size of tank becomes an important but complicated question. Taking a place with 24 inches annual rainfall we have evidently an allowance for a regular consumption of 2 inches per month. But there may be a drought in which for one month no rain falls, and the tank must have 2 inches in store to supply the deficiency. There may also be a wet month with 6 inches of rain, and as only 2 inches is consumed, 4 inches must be stored. The tank must therefore hold  $2 + 4 = 6$  inches or  $\frac{1}{4}$ th of the annual rainfall. Again, for two months we require 4 inches but the rainfall varies from  $1\frac{1}{2}$  to  $7\frac{1}{2}$  inches, and the tank must hold  $(4 - 1\frac{1}{2}) + (7\frac{1}{2} - 4) = 6$  inches as before. For three months we require 6 inches, but the rainfall varying from 2.4 to 8.7 inches, the tank should hold  $(6 - 2.4) + (8.7 - 6) =$

6 3 inches. From all this we find that a rain water tank should hold at least  $\frac{1}{4}$ th of the annual rainfall. Thus, with 24 inches, or 2 feet per year a building 1830 square feet in area, collects  $1830 \times 2 = 3660$  cubic feet, allowing a consumption of 10 cubic feet or 62 3 gallons per day, and the tank should hold  $3660 - 4 = 915$  cubic feet.

(88) "Weight and Pressure of Water"—A gallon of water at  $62^{\circ}$  weighs 10 lbs., and contains 277 274 cubic inches, or 16046 cubic foot bence a cubic foot weighs 62 321 lbs., and contains 6 2321, or nearly 6 $\frac{1}{2}$  gallons. Table 28 gives the pressure in pounds per square inch due to given columns of water and mercury.

TABLE 28.—OF EQUIVALENT PRESSURES in POUNDS per SQUARE INCH FEET of WATER, and INCHES of MERCURY at a Temperature of  $62^{\circ}$  Fahr.

Pounds per Square Inch	Feet of Water	Inches of Mercury	Pounds per Square Inch	Feet of Water	Inches of Mercury
1	2 311	2 046	2 5962	6	5 31193
2	4 622	4 092	3 0289	7	6 19731
3	8 933	6 138	3 4616	8	7 0864
4	9 244	8 184	3 8942	9	7 9697
5	11 555	10 230	48575	1 12952	1
6	13 866	12 276	97750	2 25904	2
7	16 177	14 322	1 46675	3 38856	3
8	18 488	16 368	1 95500	4 51803	4
9	20 800	18 414	2 41375	5 04 60	5
43 <sup>97</sup>	1	88333	2 93250	6 712	6
8654	2	1 77066	3 42125	7 90664	7
1 2981	3	2 65599	3 91000	9 03616	8
1 7308	4	3 54132	4 39875	10 16368	9
2 1635	5	4 41665			

EXAMPLE.—Required the Pressure per Square Inch and Equivalent Column of Mercury for a Head of 247 feet of Water.

Feet of Water	Pounds per Square Inch	Inches of Mercury
200	= 86 51 or	177 060
40	= 17 308	33 413
7	= 3 079	6 197
247	= 106 877	218 676





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FALL IN "FEET" PER MILE.

2	3	4	5	6	7	8	9
01364	02015	02727	03109	04031	04773	05151	06130

HOLE CROSS-SECTIONAL AREA IN FEET PER MINUTE.

31 5	42 3	48 8	51 6	59 8	61 6	69 1	73 2
48 8	59 8	69 1	77 2	81 6	91 4	97 7	103
59 8	73 2	81 6	91 6	101	112	120	127
69 1	81 6	97 7	103	120	129	138	146
77 2	91 6	103	122	131	144	154	161
84 6	103 6	120	131	147	153	169	179
91 4	111 9	123	144	158	171	183	194
97 7	119 6	138	154	169	183	195	207
103 6	126 9	146	161	179	194	207	220
109 2	133 7	154	173	189	201	218	232
114 5	140 3	162	181	198	214	229	243
119 6	146 5	169	189	207	224	239	254
124 5	152 5	176	197	216	233	249	264
129 2	158 3	163	204	224	212	238	274
133 8	163 8	169	211	232	250	267	284
138 1	169 2	195	218	239	258	276	293
142 4	174 4	201	225	247	266	285	302
146 5	179 4	207	232	251	274	293	311
150 5	181 4	213	238	261	282	301	319
154 4	189 1	218	241	267	289	309	328
162 0	198 4	229	256	281	303	324	344
169 2	207 2	239	267	293	316	338	359
176 1	215 6	249	278	305	329	352	374
182 7	223 8	258	289	317	342	365	388
189 2	231 7	267	299	328	354	378	401
195 4	239 3	276	309	338	365	391	414
201 4	246 6	285	318	349	377	403	427
207 3	253 8	293	328	359	388	414	440
212 8	260 7	301	337	369	398	425	452
218 2	267 5	309	345	378	409	436	463
229 0	280 5	321	362	397	429	458	486
233 2	293 2	335	378	414	448	478	508
249 0	305 2	352	394	431	466	498	528
255 4	316 6	365	403	448	483	517	548
267 6	327 6	378	423	463	500	535	567
288 8	353 9	408	457	500	540	577	611
308 8	378 3	436	488	535	578	618	655
327 6	401 3	463	518	567	613	655	695
315 4	422 9	488	516	598	616	631	733

TABLE 30 —OF THE VELOCITIES OF D

IN INCHES PER MILE AND FEET YARD

6	7	8	9	10	11	12	15	16
00341	00398	00451	00511	00568	00625	00682	00852	010

MEAN VELOCITY THROUGHOUT THE

17 3	18 6	19 9	21 1	22 3	23 4	24 4	27 3	29
21 4	26 4	28 2	29 9	31 5	33 1	34 5	38 6	42
29 9	32 3	34 5	36 6	38 6	40 5	42 3	47 3	51
31 5	37 3	39 9	42 3	44 6	46 8	48 8	51 6	59
33 6	41 7	44 6	47 3	49 8	52 3	54 6	61 9	66
42 3	45 7	48 8	51 6	54 6	57 3	59 8	66 9	73
45 7	49 4	52 8	55 9	59 0	61 9	64 6	72 1	79
48 8	52 8	56 4	59 8	63 1	66 1	69 1	77 1	81
51 8	56 0	59 8	63 4	66 9	70 1	73 3	81 9	83
54 6	59 0	63 9	66 9	70 5	73 9	77 2	86 4	91
57 8	61 9	66 1	70 1	73 9	77 5	81 0	90 6	99
59 8	64 6	69 1	73 3	77 2	81 0	84 6	91 5	103
62 8	67 3	71 9	76 3	80 4	84 3	88 1	98 4	107
64 6	69 8	74 6	79 1	83 4	87 5	91 4	102 1	111
66 9	72 2	77 2	81 9	86 3	90 6	94 6	105 7	115
69 1	74 6	79 8	81 6	89 2	93 5	97 7	109 2	119
71 2	76 9	82 2	87 2	91 9	96 4	100 7	112 5	123
73 8	79 1	84 6	89 7	94 6	99 2	103 6	115 9	126
75 3	81 8	86 9	92 2	97 2	101 9	106 4	119 9	130
77 2	83 4	89 2	91 6	99 7	104 5	109 2	122 1	133
81 9	87 5	93 5	99 2	104 6	109 8	114 5	128 9	140
84 6	91 4	97 7	103 6	109 2	111 6	119 6	133 7	146
88 1	95 1	101 7	107 8	113 6	119 2	121 5	139 2	174
91 4	98 7	105 5	111 9	118 0	123 7	120 2	141 4	154
94 6	102 2	109 2	115 8	122 1	123 1	133 7	149 5	163
97 7	105 4	112 8	119 6	126 0	132 2	138 1	151 4	170
100 7	108 7	116 2	123 3	130 0	136 3	142 4	159 2	174
103 6	111 9	119 6	126 9	133 8	140 2	146 5	163 8	181
106 3	115 0	122 9	130 4	137 4	141 0	150 5	168 3	181
109 1	117 9	126 1	133 7	141 0	147 3	151 5	172 7	181
114 5	123 7	132 3	140 3	147 9	153 0	162 0	181 1	196
119 6	129 2	138 1	146 5	151 4	161 9	169 2	189 1	20
121 5	131 5	143 8	152 5	160 7	168 0	176 4	186 9	-1
129 2	139 5	149 2	159 3	166 8	175 0	182 7	201 3	2
133 8	144 1	151 5	163 8	172 7	181 1	189 2	211 5	21
141 4	156 0	166 8	176 9	186 5	195 5	203 8	228 4	236
151 4	166 8	178 3	189 1	199 3	209 1	215 -	214 2	-6
163 8	177 0	189 2	200 6	211 5	221 8	231 6	239 0	25
172 7	186 5	199 4	211 5	222 9	233 8	241 2	253 0	-





## —OF THE DISCHARGE OF PIPES BY PEONY'S FORMULA.

## DIAMETER OF THE PIPE IN INCHES.

5	6	7	8	9	10	12
GALLONS DISCHARGED PER MINUTE.						
1.278	1 841	2 501	3 272	4 142	5 113	7 5
2 556	3 682	5 003	6 514	8 281	10 23	14 2
3 831	5 523	7 512	9 516	12 43	15 31	22 6
5 113	7 373	10 02	13 09	16 57	20 45	29 4
6 390	9 205	12 52	16 56	20 71	25 57	36 5
7 668	11 03	15 02	19 63	21 85	26 67	41 1
8 947	12 85	17 53	22 93	25 90	35 79	51 5
10 23	14 73	20 01	26 18	33 13	40 91	58 4
11 50	16 57	22 51	29 45	37 28	46 02	66 6
12 78	18 41	25 01	32 72	41 42	51 13	73 4
14 06	20 23	27 51	36 00	45 56	56 25	60 5
15 34	22 03	30 05	39 27	49 70	61 36	68 5
16 62	23 83	32 55	42 51	53 84	66 46	75 2
17 89	25 77	35 05	45 81	57 98	71 59	103 1
19 17	27 61	37 56	49 03	62 13	76 09	110 4
20 45	29 45	40 06	52 36	66 27	81 81	117 5
21 73	31 23	42 57	55 63	70 41	86 94	125 2
23 01	33 13	45 07	59 90	74 55	92 03	132 6
24 29	34 97	47 58	62 17	78 70	97 14	139 4
25 57	36 82	50 08	65 45	82 63	102 3	147 4
26 12	40 50	55 09	72 00	91 12	112 5	162 6
30 68	44 18	60 10	78 54	99 40	122 7	176 7
33 23	47 86	65 10	85 04	107 7	132 9	191 4
35 79	51 51	70 11	91 63	116 0	143 2	206 4
38 31	55 23	75 12	98 16	124 3	153 4	220 5
40 90	58 90	80 13	101 7	132 5	163 6	235 6
43 46	62 59	85 14	111 3	140 8	173 8	250 5
46 02	66 27	90 14	117 8	149 1	184 2	265 4
51 13	73 63	100 2	130 9	165 7	204 5	294 5
53 69	77 31	105 2	137 4	174 0	214 7	309 2
56 21	80 99	110 2	141 0	182 2	224 9	324 6
58 80	84 67	115 2	150 5	190 5	235 2	338 1
61 36	88 36	120 2	157 1	198 8	245 4	353 4
63 91	92 01	125 2	163 6	207 1	255 7	368 1
66 47	95 72	130 2	170 2	215 4	265 9	382 6
69 02	99 40	135 2	176 7	223 6	276 1	397 6
71 58	103 1	140 2	183 3	231 9	296 4	412 2
74 14	106 8	145 2	189 8	240 2	296 6	427 0
76 63	110 5	150 2	196 3	248 5	306 8	441 7

1	1½	2	2½	3	3½	4
25	0511	1150	2015	3196	4602	6000
1022	2301	4001	6392	9201	1 202	1 4
1531	3150	6136	9588	1 331	1 878	2 4
2015	4002	6182	1 278	1 811	2 501	3 2
2556	5700	1 023	1 598	2 301	3 130	4 0
5	3067	6000	1 227	1 917	2 761	3 706
75	3578	803	1 432	2 237	3 221	4 382
10	4000	9201	1 636	2 537	3 692	5 005
25	4601	1 035	1 811	2 876	4 142	5 631
1	5112	1 150	2 015	3 196	4 602	6 260
5	5621	1 265	2 250	3 515	5 062	6 896
75	6135	1 381	2 434	3 935	5 522	7 512
10	6616	1 496	2 659	4 151	5 942	8 124
25	7157	1 611	2 861	4 171	6 113	8 714
1	7603	1 726	3 008	4 791	6 903	9 300
5	8180	1 811	3 273	5 113	7 363	10 07
25	8631	1 935	3 177	5 473	7 897	10 61
1	9202	2 071	3 682	5 757	8 251	11 27
15	9713	2 186	3 896	6 077	8 741	11 89
1	1 023	2 301	4 001	6 392	9 201	12 52
5	1 125	2 531	4 700	7 031	10 12	13 77
1	1 227	2 761	4 900	7 670	11 01	15 0
5	1 329	2 991	5 918	8 300	11 96	16 48
1	1 431	3 221	5 727	8 918	12 88	17 59
1	1 533	3 450	6 136	9 598	13 81	18 78
5	1 636	3 682	6 514	10 23	14 73	20 01
1	1 738	3 912	6 954	10 84	15 65	21 59
1	1 841	4 142	7 363	11 51	16 57	22 53
2	2 015	4 602	8 182	12 78	18 41	23 01
2	2 147	4 832	8 591	13 42	19 33	- 29
2	2 219	5 062	9 000	14 06	20 25	27 1
2	2 351	5 292	9 409	14 70	21 15	28 60
2	2 451	5 522	9 818	15 34	22 09	30 05
2	2 556	5 753	10 23	15 94	23 01	31 59
2	2 658	5 983	10 61	16 62	23 7	31 53
2	2 761	6 213	11 01	17 26	21 81	27 89
2	2 863	6 443	11 45	17 90	22 77	28 01
2	2 955	6 673	11 8	18 71	23 69	27 1
3	3 07	6 899	12 7	19 14	27 11	29 0

-OF THE DISCHARGE OF PIPES BY PROVY'S FORMULA.

DIAMETER OF THE PIPE IN INCHES.

5	6	7	8	9	10	12
GALLONS DISCHARGED PER MINUTE.						
1 278	1 841	2 504	3 272	4 142	5 113	7 1
2 556	3 682	5 003	6 544	8 284	10 23	14 2
3 834	5 523	7 512	9 816	12 43	15 34	22 2
5 113	7 363	10 02	13 00	16 57	20 45	29 4
6 390	9 205	12 52	16 36	20 71	25 57	36 5
7 668	11 05	15 02	19 63	24 85	30 67	41 1
8 947	12 88	17 53	22 95	28 90	35 79	51 2
10 22	14 73	20 03	26 18	33 13	40 91	58 5
11 50	16 57	22 54	29 45	37 28	46 02	66 2
12 78	18 41	25 04	32 72	41 42	51 13	73 6
14 66	20 25	27 54	36 00	45 56	56 25	80 6
15 34	22 09	30 05	39 27	49 70	61 36	83 2
16 02	23 93	32 55	42 51	53 81	66 46	95 2
17 83	25 77	35 06	45 81	57 99	71 59	103 1
19 17	27 61	37 56	49 03	62 13	76 69	110 4
20 45	29 45	40 06	52 36	66 27	81 81	117 2
21 73	31 30	42 57	55 03	70 41	86 94	125 2
23 01	33 13	45 07	58 90	74 55	92 03	132 2
24 29	34 97	47 53	62 17	78 70	97 11	139 2
25 57	36 82	50 08	65 45	82 83	102 3	147 2
26 12	40 50	55 09	72 00	91 12	112 5	162 6
28 03	44 18	60 10	78 51	95 49	122 7	176 2
33 23	47 86	63 10	85 04	107 7	132 9	191 4
35 79	51 54	70 11	91 63	116 0	143 2	227 1
38 34	55 23	75 12	99 16	124 3	153 4	229 2
40 50	59 90	80 13	104 7	132 5	163 5	231 6
43 45	62 59	85 11	111 3	140 8	173 8	239 2
46 02	66 27	90 14	117 8	149 1	184 2	265 1
51 13	73 63	100 2	120 9	163 7	204 5	291 2
53 69	77 31	105 2	127 4	174 0	214 7	299 2
56 24	80 29	110 2	141 0	192 2	224 9	321 6
58 80	84 87	115 2	150 5	199 5	225 2	327 4
61 36	89 26	120 2	157 1	204 8	235 4	334 1
63 91	92 04	125 2	162 6	207 1	235 7	332 4
66 47	95 72	130 2	179 2	213 4	245 9	339 2
69 02	99 40	135 2	176 7	227 7	277 1	357 6
71 53	103 1	140 2	182 3	231 2	284 4	412 2
74 14	107 8	145 2	189 2	232 2	284 7	417 2
75 63	110 5	150 2	194 3	244 5	294 4	411 2



Fig. 11

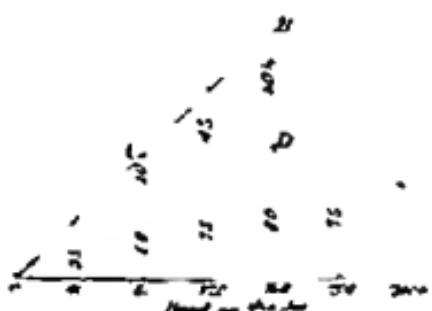


Fig. 15

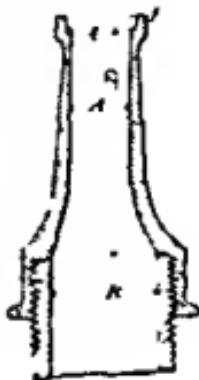


Fig. 16

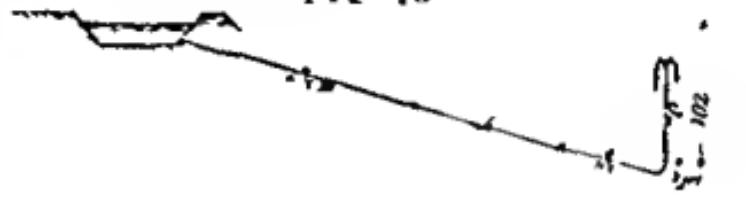


Fig. 17



Fig. 18

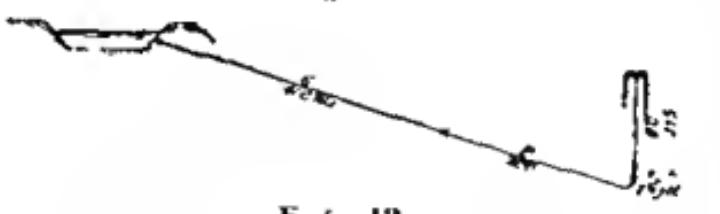
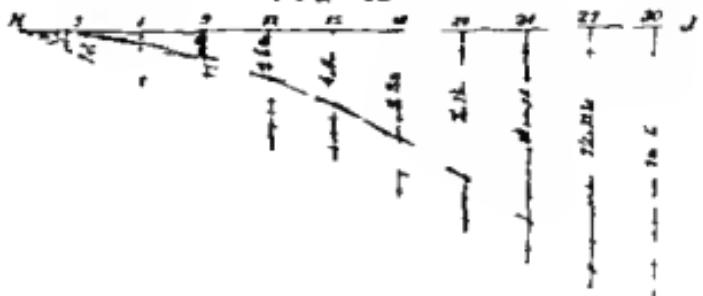


Fig. 19





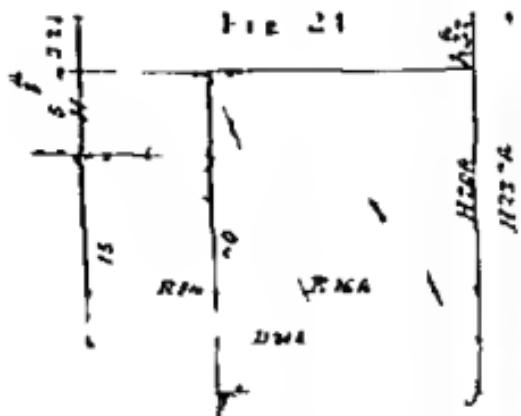
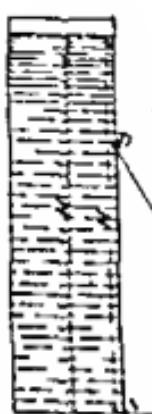


Fig. 26

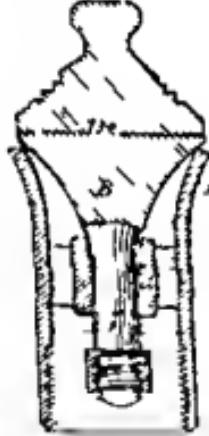
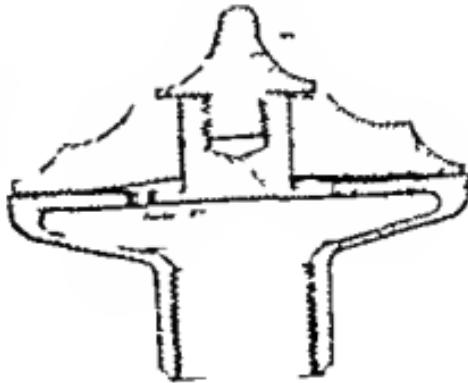


Fig. 27



Fig. 28





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